

Hydraulic calibration of wastewater treatment plants as a key tool for the evaluation and comparison of the removal efficiencies of contaminants of emerging concern



Zeina Baalbaki*, **Frédéric Cloutier****, **Peter A. Vanrolleghem**** and **Viviane Yargeau***

* Yargeau 3Cs Laboratory, Chemical Engineering Department, McGill University

** modelEAU, Département de génie civil et de génie des eaux, Université Laval



YARGEAU LABORATORY

Controlling
Contaminants of
Concern



McGill

Contents

- ✧ **Background**
- ✧ **Problem statement and objectives**
- ✧ **Methodology**
- ✧ **Collected data**
- ✧ **Best-fit model**
- ✧ **Load fractions**
- ✧ **Results summary**
- ✧ **Application to chemical analysis**
- ✧ **Conclusions & further research**
- ✧ **Acknowledgements**



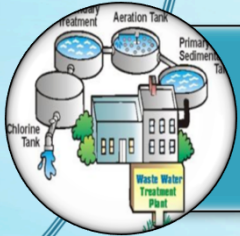
Background



Several contaminants of emerging concern (CECs) are detected in surface water



These contaminants are discharged to the environment from wastewater treatment plants (WWTPs)



It is essential to understand the removal of CECs during wastewater

Contaminants of Emerging Concern (CECs)



Persistent organic pollutants



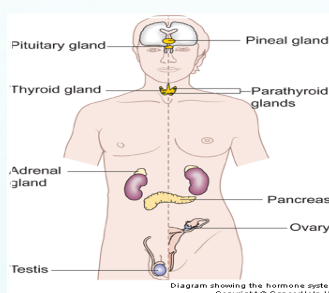
Pharmaceuticals and illicit drugs



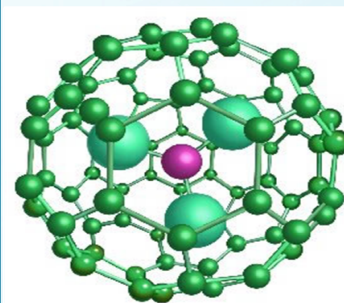
Personal Care products



Veterinary medicines



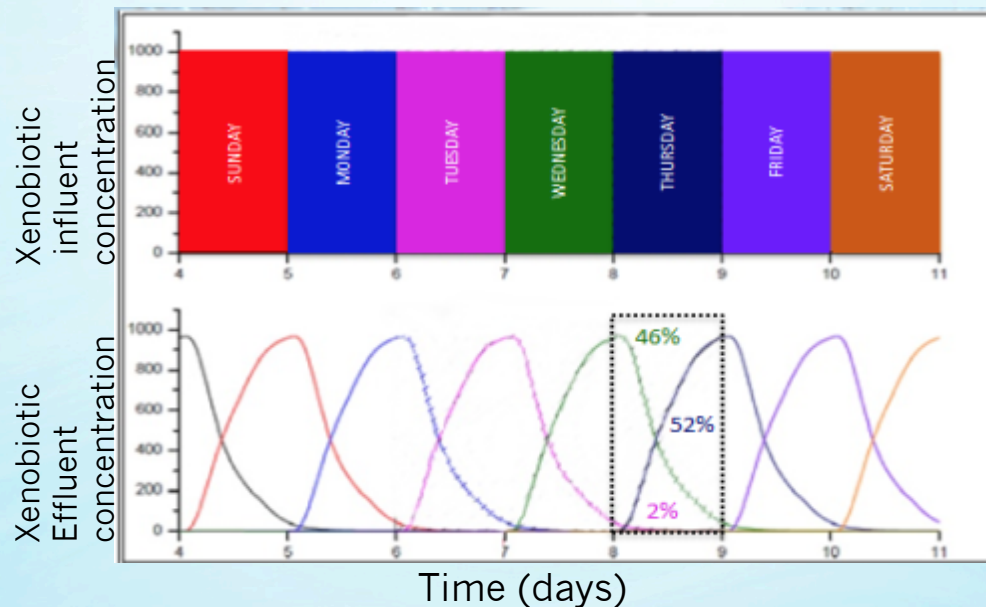
Endocrine disrupting compounds (EDCs)



Nanomaterials

Problem statement

- ✧ The conventional way to determine removal of CECs compares influent and effluent loads on the same day
→ might lead to unreliable and even negative removals due to mismatch of loads
- ✧ The effluent on a certain day contains influent load from several past day due to residence time distribution (RTD)



Calculation of removal efficiency

✧ Conventional approach

$$E = \frac{L_{inf} - L_{eff}}{L_{eff}} \times 100 \%$$

✧ Proposed approach taking RTD into consideration

$$E = \frac{L_{ref} - L_{eff}}{L_{eff}} \times 100 \%$$

L_{eff} : Output measured load on one day

E : Removal efficiency

$$L_{ref} = \sum_{i=1}^n f_n L_n$$

L_{ref} : The output load considering the RTD and without any removal

f_n : Load fraction of each day

L_n : Measured load from each day

Objectives

- ✧ Use hydraulic calibrations for selected WWTPs to understand the differences in the hydraulic behavior and its impact on the calculation of CECs removals

Ville de Granby Québec

- Population of 54,000
- Treats around 50,260 m³/day

City of Peterborough Ontario

- Population of 78,700
- Treats around 43,000 m³/day

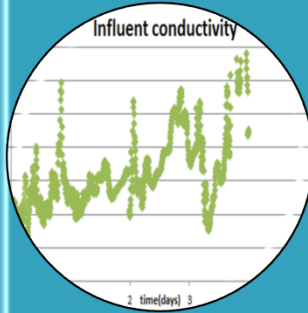
City of Guelph Ontario

- Population of 120,000
- Treats around 60,000 m³/day

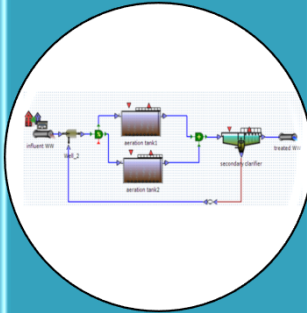
Methodology



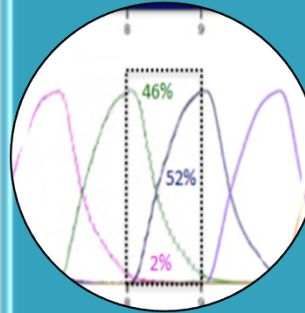
Deploy electroconductivity (EC) probes and collect composite samples around the activated sludge unit of the 3 WWTPs



Use EC as a tracer as a indicator of the residence time distribution



Model the aeration tank as different number and arrangement of aeration tanks using WEST software



Use the model to find effluent load fractions from past days

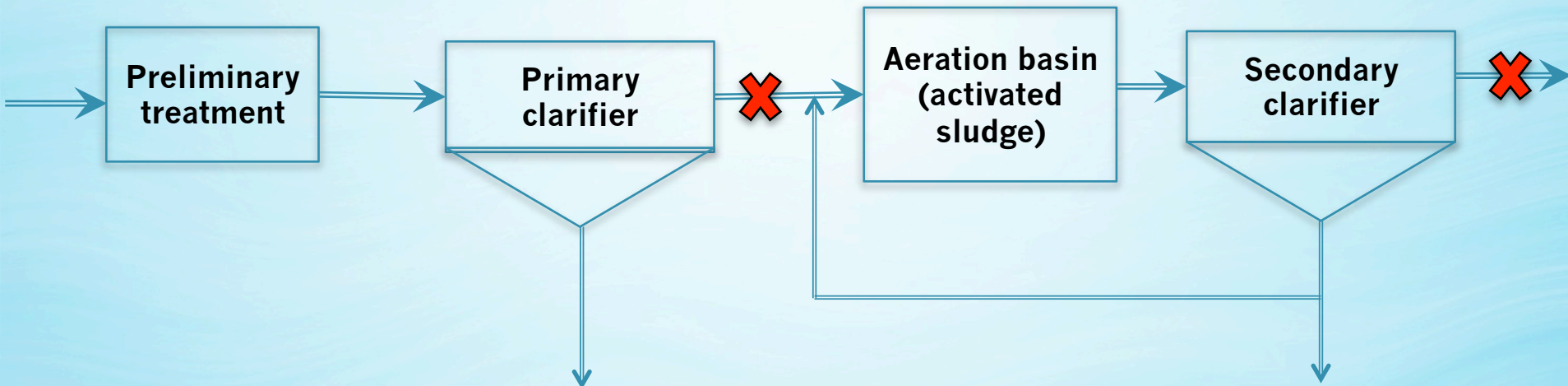


Use load fractions and chemical analysis (LC-MS/MS) to find the removal of CECs by activated sludge unit



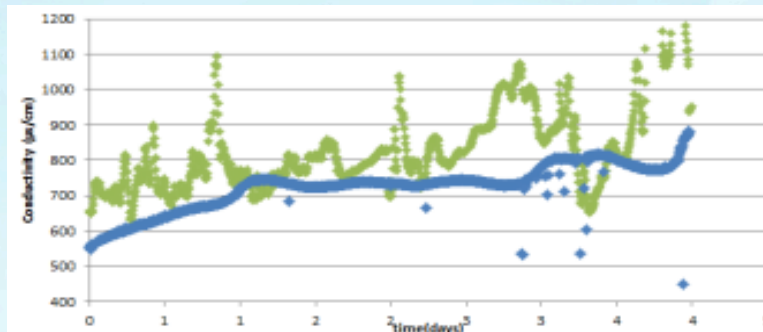
Electroconductivity as a tracer

- ✧ It is not practical to inject an inert in the water of multiple WWTPs to model their RTD
- ✧ Conductivity changes between influent and effluent of activated sludge unit, or other units, is then used to trace the hydraulic behavior



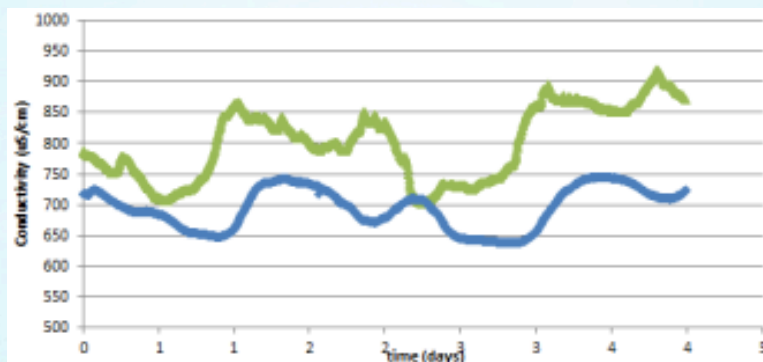
Collected conductivity trends

✧ Granby



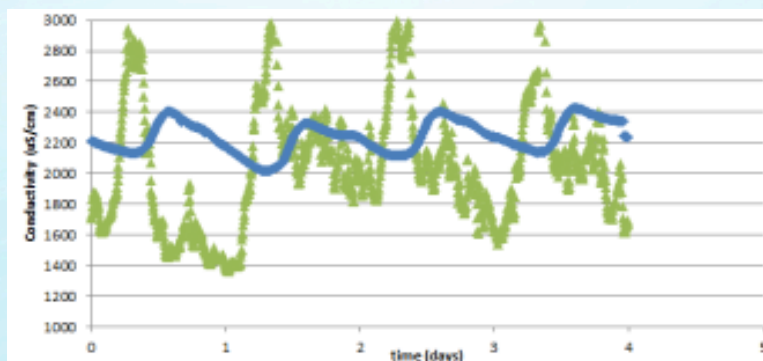

Influent
Sharp signal

✧ Peterborough



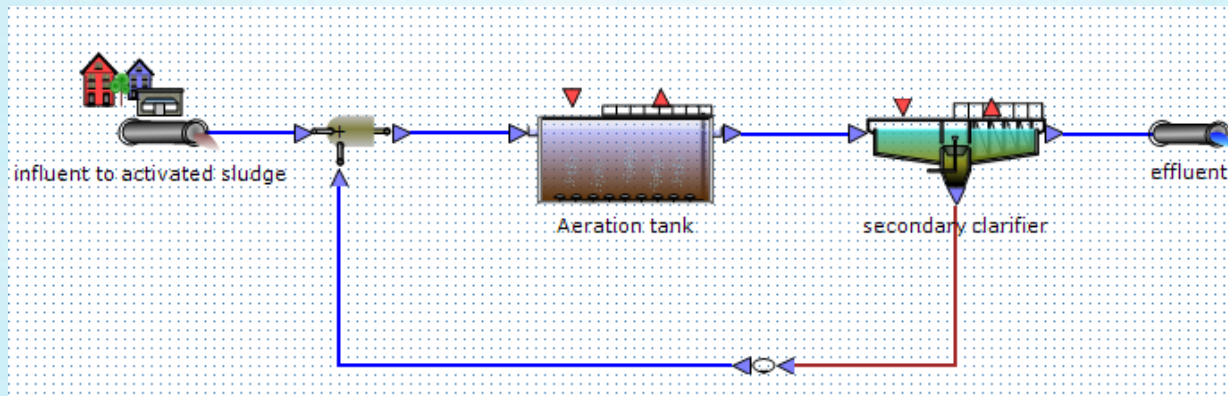
Effluent
distributed and shifted
response

✧ Guelph



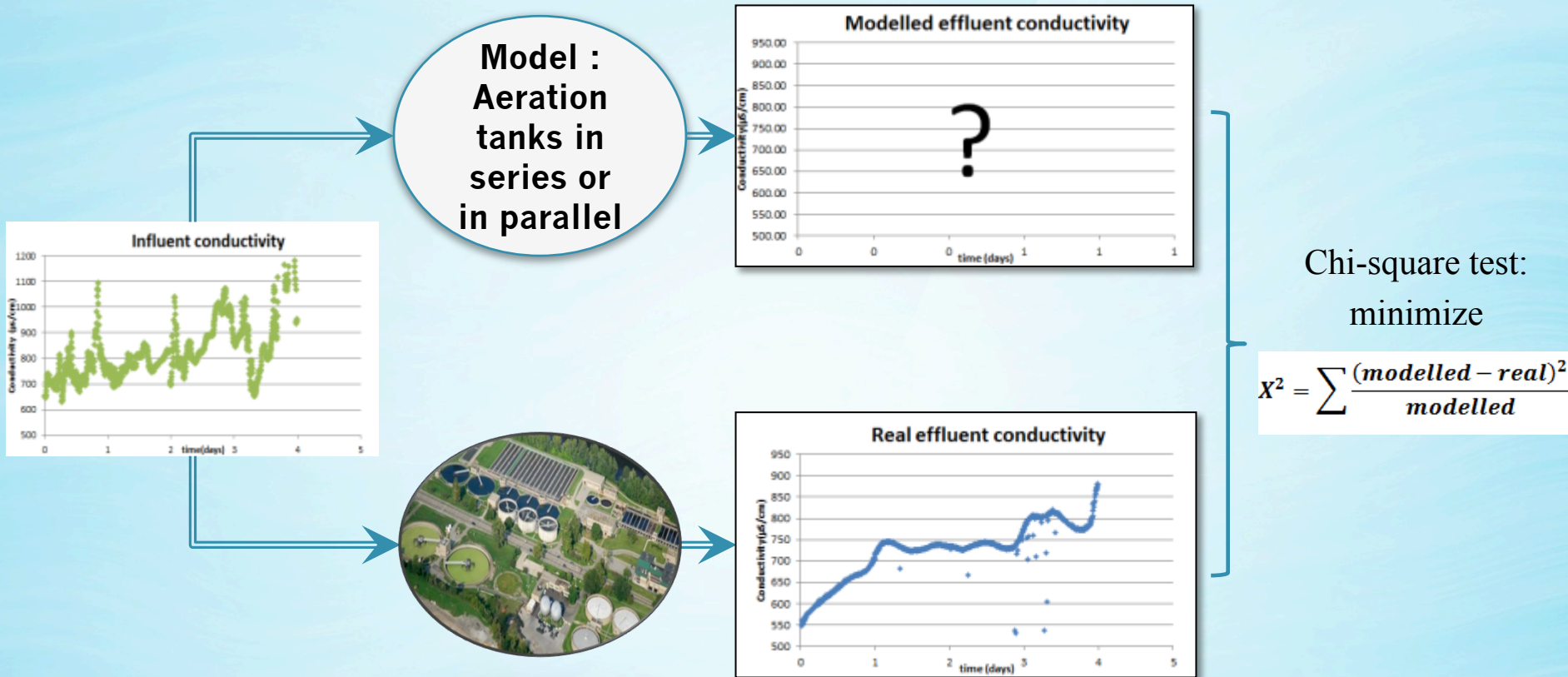
Modelling using WEST

- ✧ Real influent data are inputted to the model
- ✧ The base case consists of one aeration tank and one secondary clarifier, both with the same actual total volume



- ✧ Aeration tanks are added in series or parallel, to create various RTD models but the total volume of aeration tanks is kept the same
- ✧ Dynamic simulation is carried out on 4 days (same as EC probes deployment period)

Choose the best RTD model

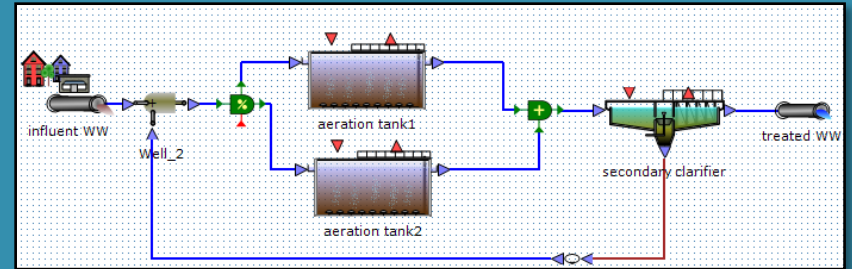


✧ The different models tested represent different residence time distribution (RTD) patterns

Results for the best models

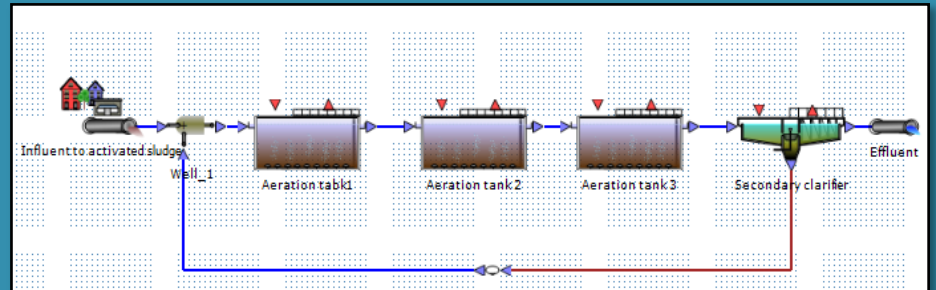
Granby

- Two aeration tanks in parallel



Guelph

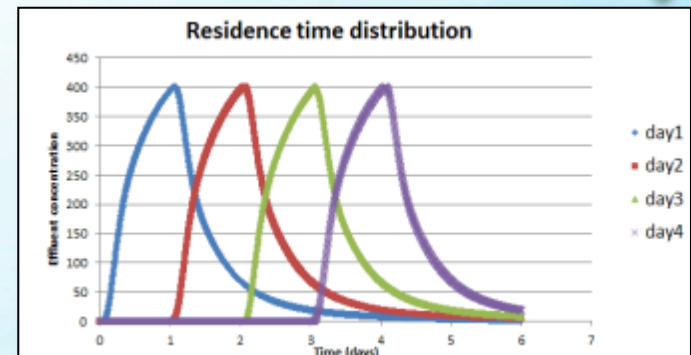
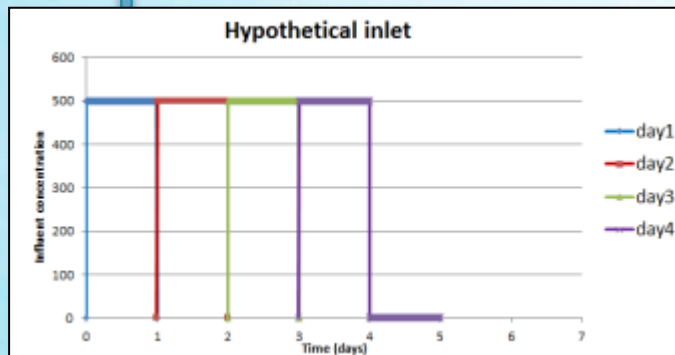
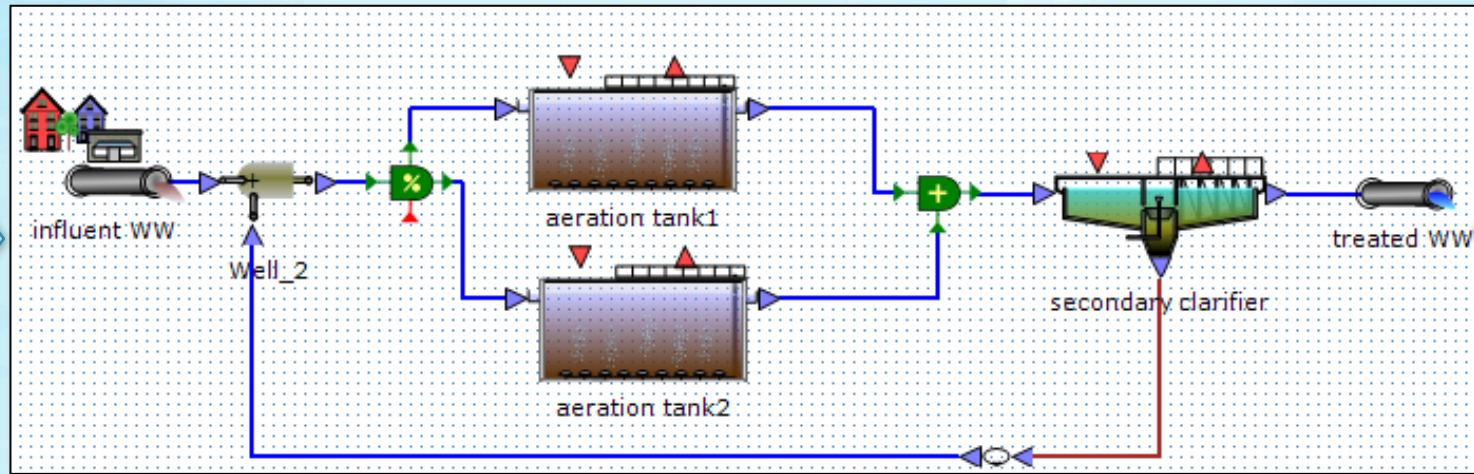
- Three aeration tanks in series



Peterborough

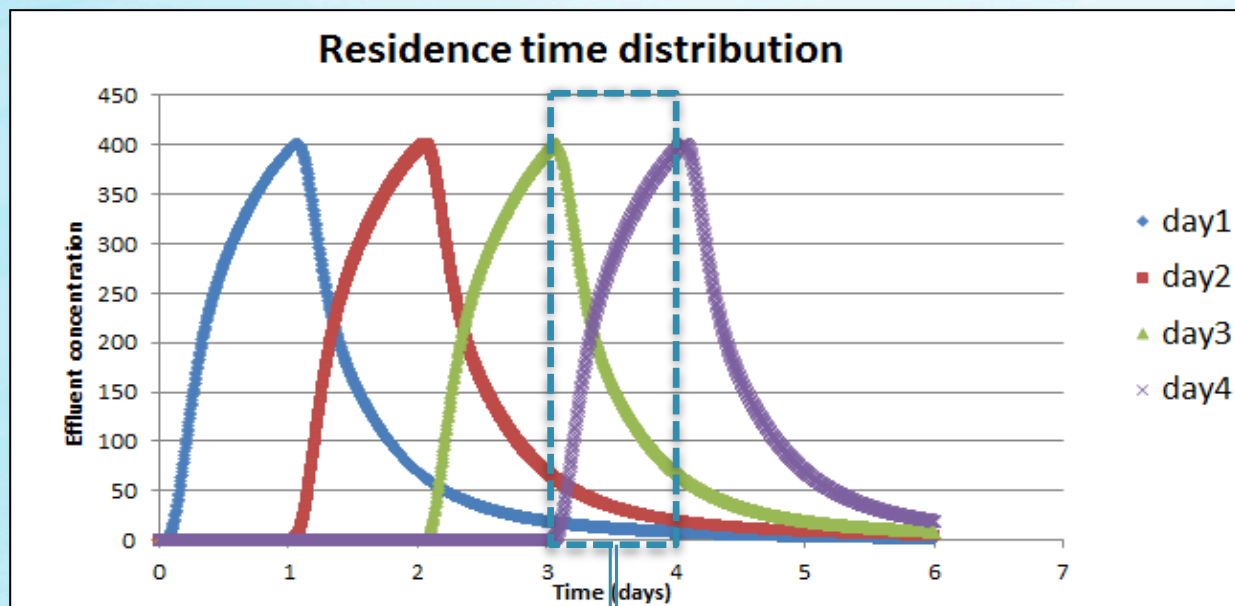
- Infinite aeration tanks in series or PFR because effluent is only time shift of influent

Obtaining load fractions – Granby



Obtaining load fractions – Granby

- ✧ The fractions are found as the fraction of the area under each curve in the box of a given day



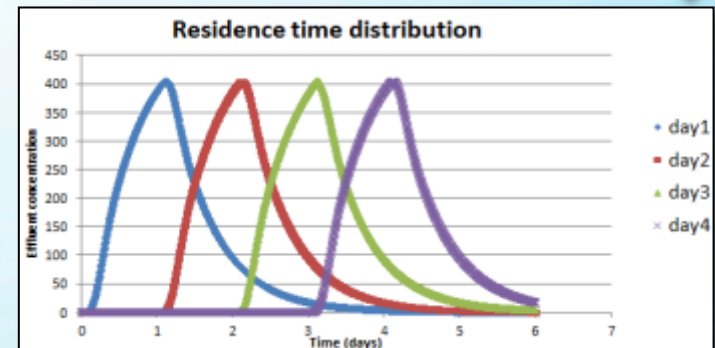
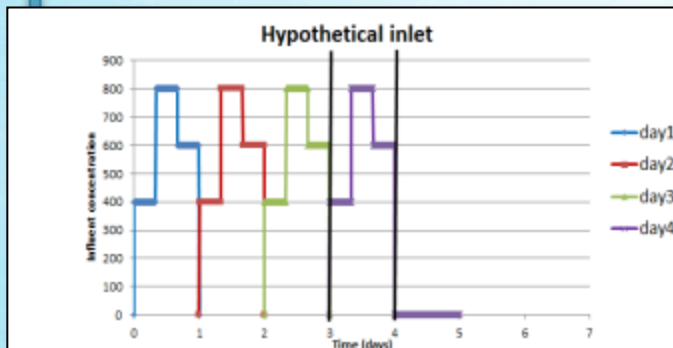
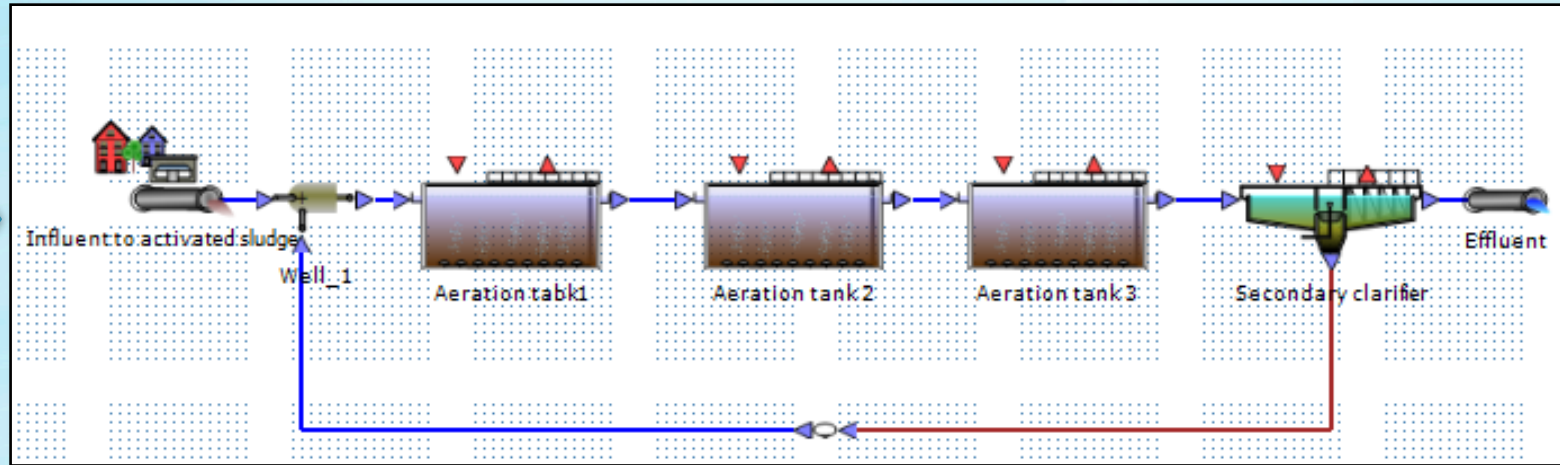
Indicates that the effluent on day 4 is composed of: **49% day 4 (same day)**

41% day 3

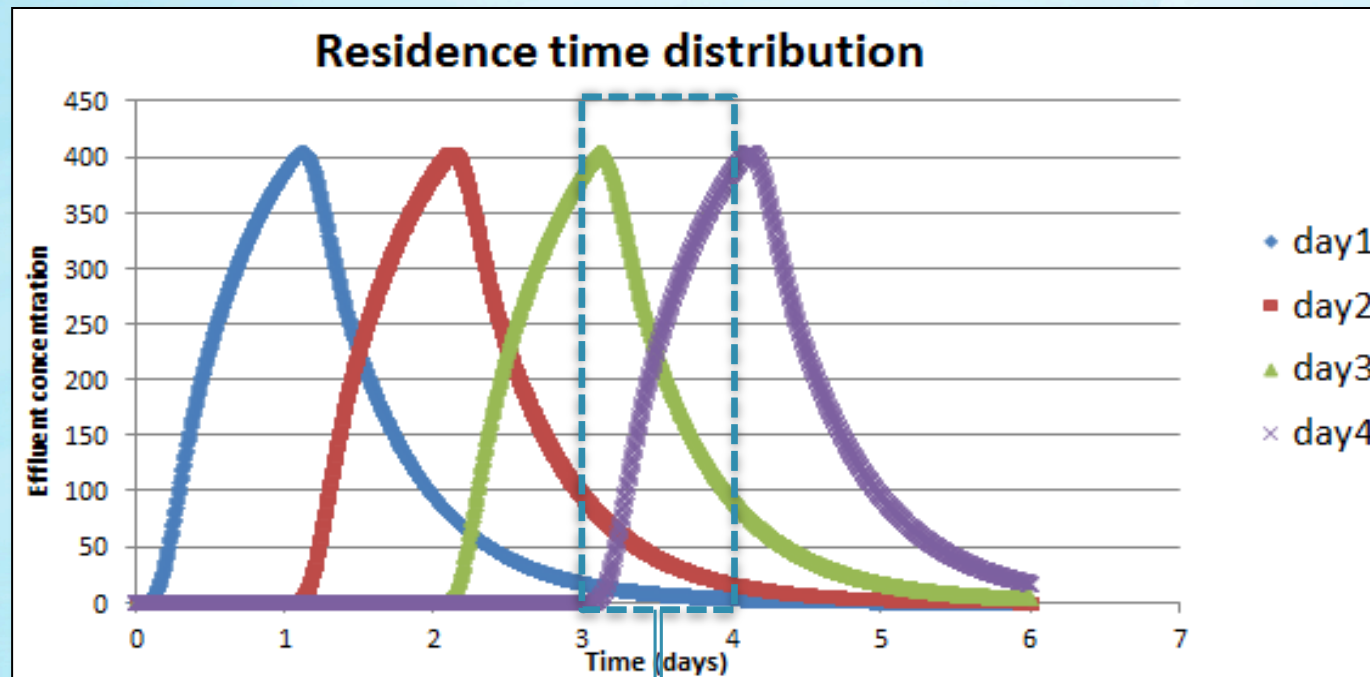
8% day 2

3% day 1

Obtaining load fractions – Guelph



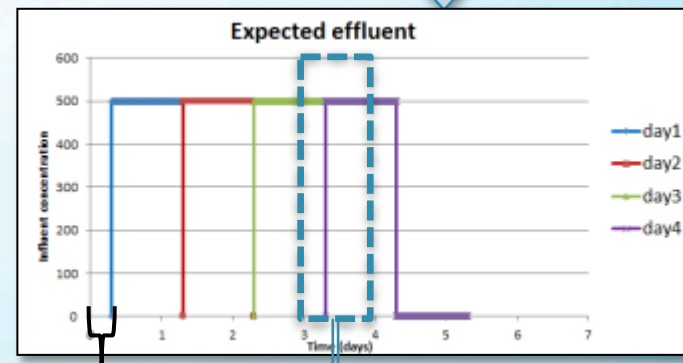
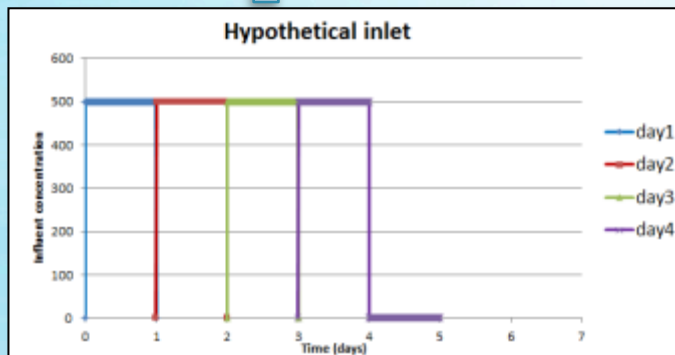
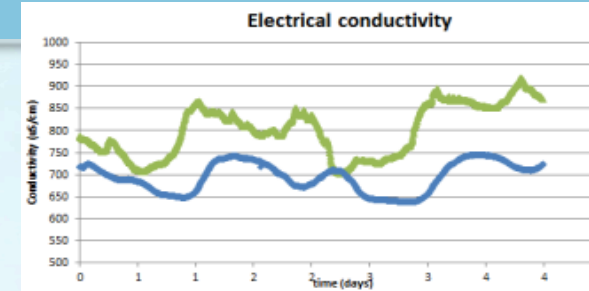
Obtaining load fractions – Guelph



Indicates that the effluent on day 4
is composed of: **40% day 4 (same day)**
49% day 3
9% day 2
2% day 1

Obtaining load fractions - Peterborough

- Due to the absence of RTD as plug flow reactor (PFR) → WEST not needed
- The effluent on one day contains load from only one past day and the fractions depend on the time constant of the activated sludge unit



$\tau=0.3$ days

70% day 4 (same day)
30% day 3

Calculations of removal

✧ Example of Granby

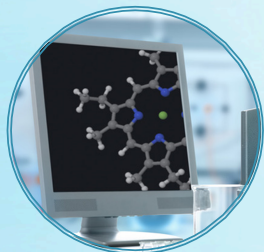
- Concentrations were determined by LC-MS\MS
- Removal efficiencies were using the conventional method and the time-shifted approach

Compound	Day	Day-by-day removal (%)	Time-shifted removal (%)
Ephedrine	1	85%	86%
	2	91%	
	3	90%	
	4	85%	
Methadone	1	-29%	42%
	2	55%	
	3	37%	
	4	48%	

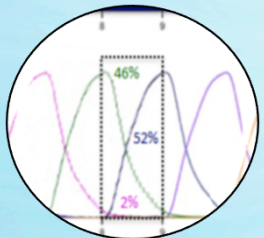
Location	Day	Ephedrine (ng/L)	Methadone (ng/L)
Influent	1	558	9
	2	982	23
	3	1019	16
	4	946	21
Effluent	1	87	12
	2	93	10
	3	103	10
	4	139	11

Conclusions and further steps

- ✧ The three activated sludge plants proved to have different mixing regimes, which significantly affect the transport of contaminants in the activated sludge unit.
- ✧ The residence time distribution is critical in properly evaluating the removal of contaminants



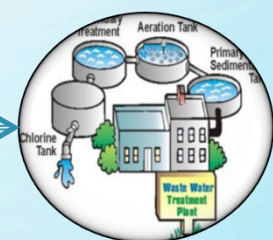
Chemical
analysis



Hydraulic
calibration



Reliable CECs
removal data



Model to predict
CECs removal
as a design tool

Acknowledgements

- ✧ **Prof. Viviane Yargeau**
- ✧ **Laval University for training on WEST Software**
- ✧ **3Cs group**
- ✧ **McGill Engineering Doctoral Award (MEDA)**
- ✧ **NSERC Strategic Projects Program for funding**

Questions



Summary of results

✧ Granby

- Best model is 2 tanks in parallel
- Effluent is composed of 49% day-4 (same day), 41% day-3, 8% day-2, 3% day-1

✧ Peterborough

- Best model is PFR
- Effluent is composed of 70% day-4 (same day), 30% day-3

✧ Guelph

- Best model is 3 tanks in series
- Effluent is composed of 40% day-4 (same day), 49% day-3, 9% day-2, 3% day-1