



DIPARTIMENTO DI SISTEMI E INFORMATICA  
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## **AVVISO DI SEMINARIO**

Giovedì 25 Novembre p.v. alle ore 9:00  
nell'Aula Seminari del Dipartimento di Energetica "Sergio Stecco" (g.c.)  
primo piano, lato Est.

**Il Prof. Peter Vanrolleghem**

### **On-line characterization of waste load and toxicity with activated sludge respirometry**

Abstract

Respirometry, the measurement of the oxygen consumption by organisms for substrate degradation and cell maintenance, has become one of the key monitoring techniques in wastewater treatment.

After some introduction on the different respirometric measuring principles, focus of the presentation will be put on the on-line application of batch-wise operating respirometers on full-scale plants. They allow to characterize the waste load (BOD<sub>st</sub> and substrate fractions, including nitrifiable nitrogen) and potential toxicity of influents.

The usefulness and current implementation in wastewater treatment plant control will be discussed.

IAWQ Scientific and Technical Report (STR)

# Respirometry in Control of the Activated Sludge Process

Henri Spanjers

Peter Vanrolleghem

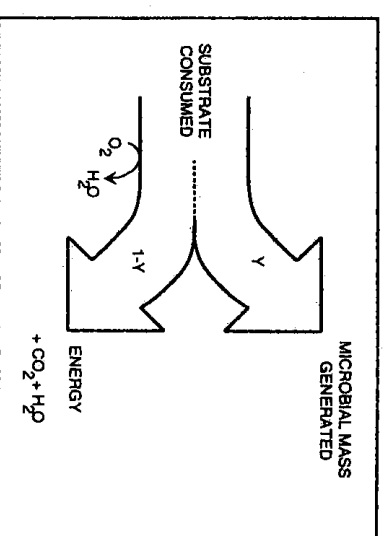
Gustaf Olsson

Peter Dold

WQI '96, Singapore, 23-28 June

1

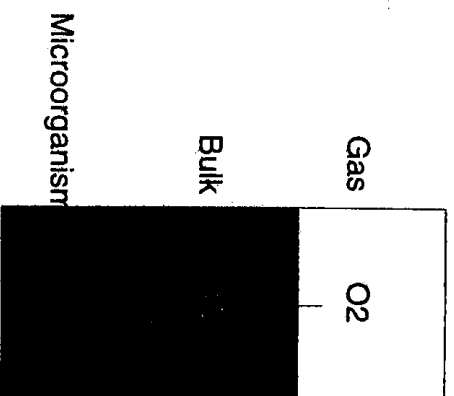
## Substrate consumption



WQI '96, Singapore, 23-28 June

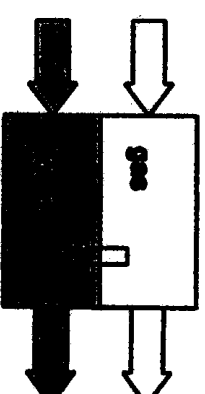
Background 2

## Respirometers



- Respiration takes place in liquid
- Uptake of DO from liquid
- Transfer of O<sub>2</sub> from gas to liquid
- Dynamic oxygen mass balance

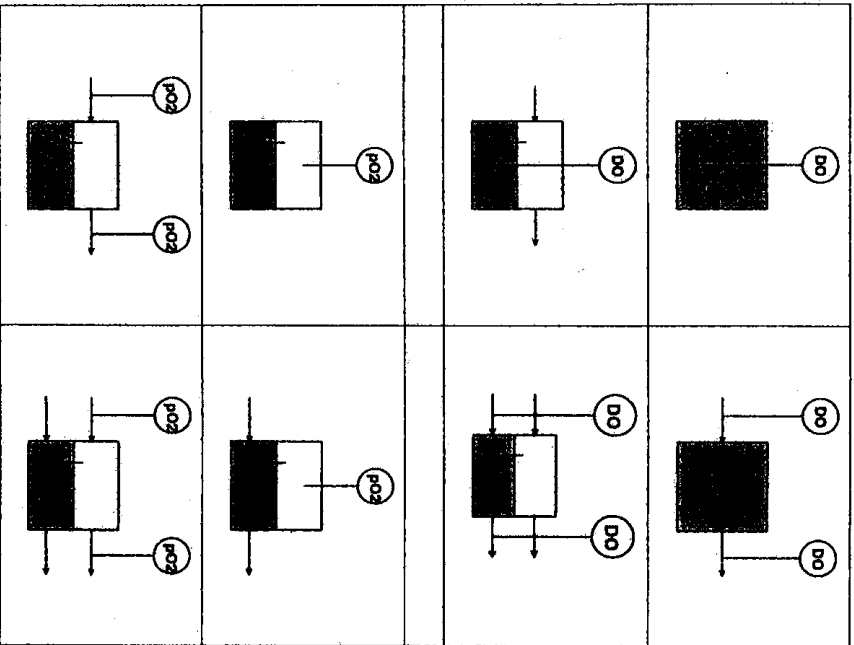
## Generic Respirometer



Phase of Oxygen measurement: Gas or Liquid

Flow regime: Static or Flowing

## Eight different principles



## Liquid phase principles

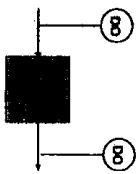
**LSS** no gas flow, no liquid flow

$$\frac{dC_L}{dt} = -r$$



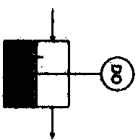
**LSF** no gas flow, with liquid flow

$$\frac{dC_L}{dt} = \frac{Q}{V_L} (C_{L,in} - C_L) - r$$



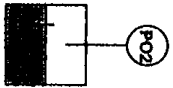
**LFS** with gas flow, no liquid flow

$$\frac{dC_L}{dt} = K_L a (C_L^* - C_L) - r$$



# Gas phase principles

**GSS** no gas flow, no liquid flow;  
constant V



$$\frac{dC_L}{dt} = K_L a (C_L^* - C_L) - r$$

$$\frac{dC_G}{dt} = - \frac{V_L}{V_G} K_L a (C_L^* - C_L)$$

WQ1 '96, Singapore, 23-28 June

Principles 9

# Summary Respirometric Principles

respirometric principle - process 1	liquid phase				gas phase			
	LSS	LSF	LFS	LFF	GSS	GSF	GFS	GFF
respiration	-1	-1	-1	-1	-1	-1	-1	-1
dissolved oxygen accumulation		-1	-1	-1	-1	-1	-1	-1
liquid volume change			-1	-1		-1		-1
liquid flow			1	1		1		1
gas exchange				1		1	1	1
gaseous oxygen accumulation					-1	-1	-1	-1
gas volume change					-1	-1	-1	-1
gas flow							1	1
gas exchange					-1	-1	-1	-1

## Introduction

### OXYGEN:

a Key Variable In Wastewater Treatment

- ① - COD Removal                      -> Effluent Quality
- Nitrification
- ② - Aeration Cost                    -> Economy

### MICROBIAL RESPIRATION RATE

a Look at the Interaction between                      - Wastewater  
providing insight in:    - Biocatalysts

- Composition
- Biodegradability
- Degradation Rate
- Adaptation Time
- Toxicity (Acute & Chronic)
- Sludge Viability/Activity  
(Actual/Potential)

## On-line Influent Composition Assessment

### WHY ?

Knowledge on Future Load Variations  
Knowledge on Future Potential Toxicity

-> Feedforward Control

### WHERE ?

As far Upstream of the Works as possible  
and still Provide Relevant Information

### HOW ?

Chemical: TOC, COD, TOD

Physical: Conductivity, UV-absorption

Advantages:    Fast  
                    Standardized

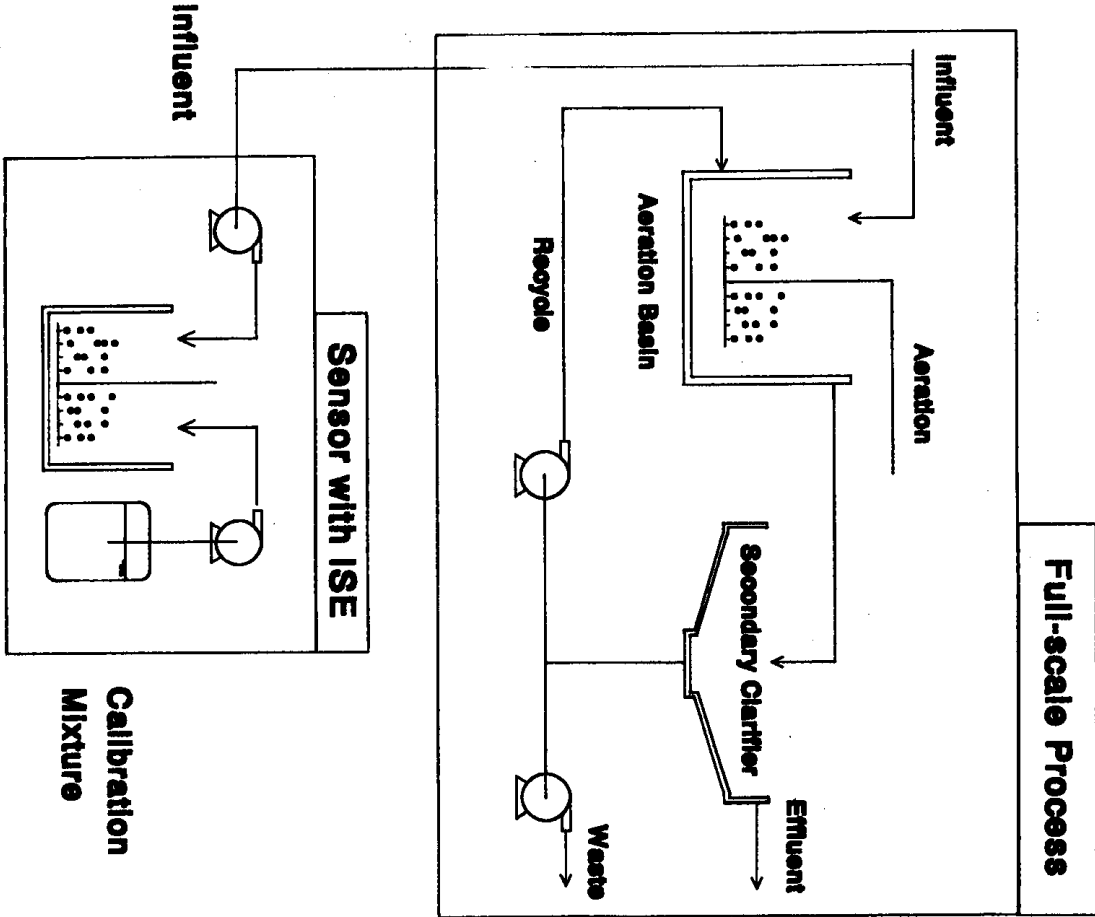
Disadvantages: Maintenance  
                    Biodegradability  
                    Toxicity

Biological: BOD<sub>5</sub>

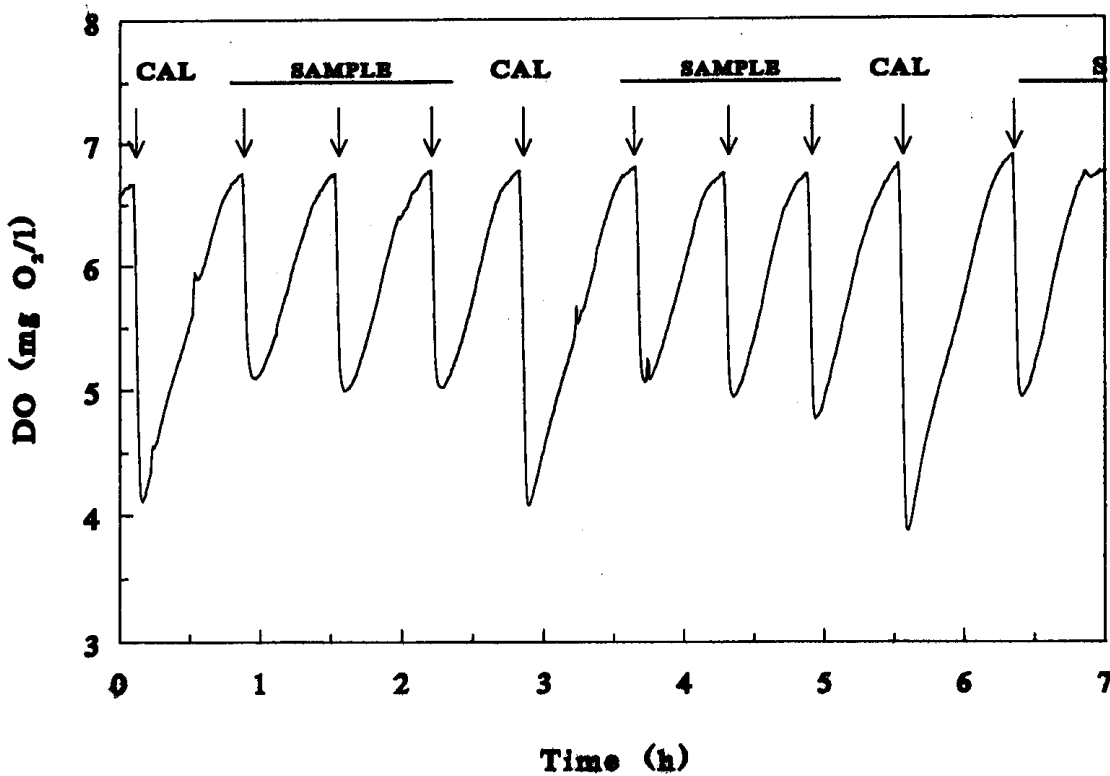
Advantages:    Biodegradability  
                    Toxicity

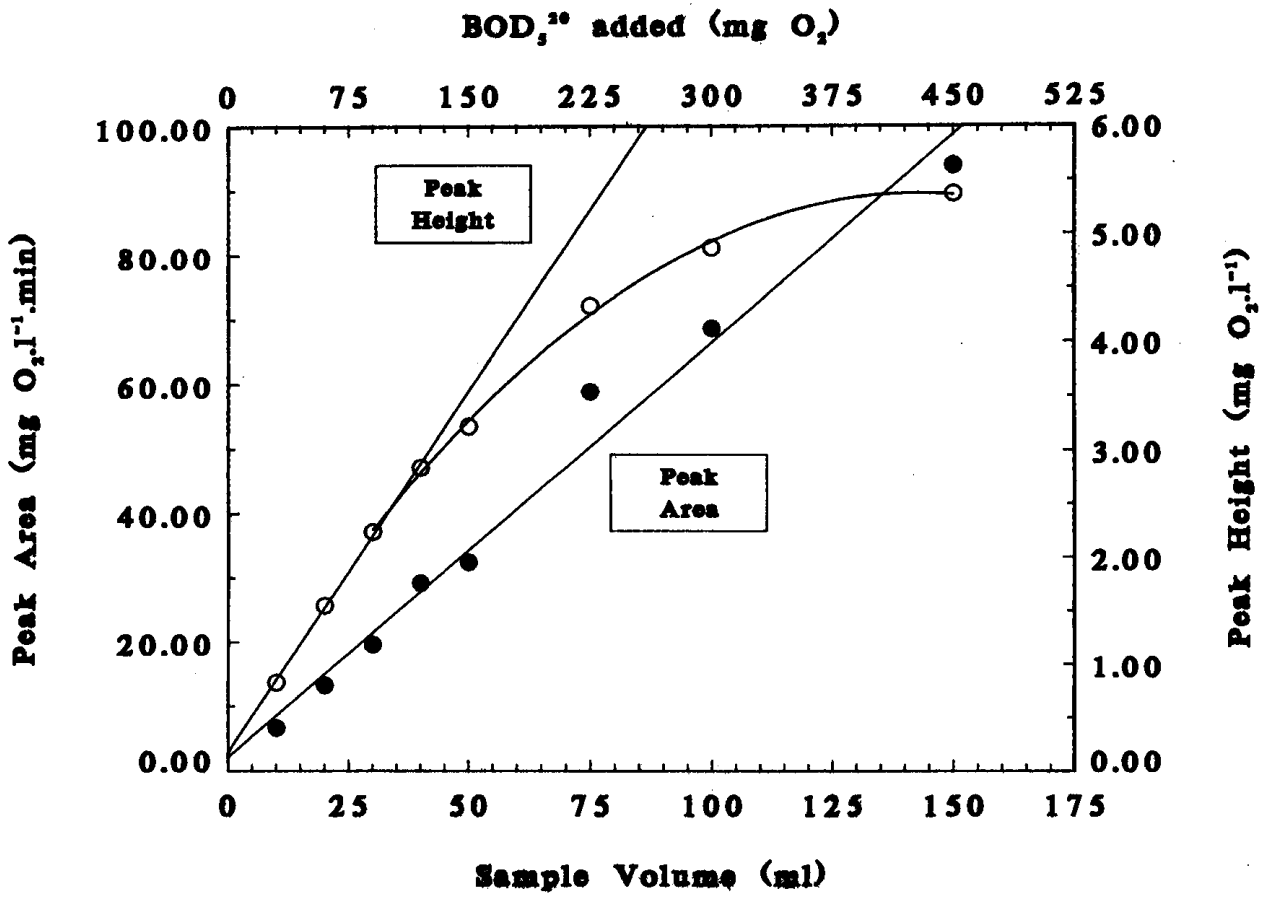
Disadvantage: Slow                      -> BOD<sub>5</sub>

# In-Sensor-Experiments



## Typical RODTOX Respirogram Run





## BOD<sub>a</sub> Calculation

### General

$$BOD_a = \int_0^{t_{fin}} OURex(t) dt$$

Using OURex(t) Profiles Generated with Both Principles

-> BOD<sub>a</sub> injected in the Vessel can be Calculated

$$BOD_a(\text{sample}) = \frac{V_{\text{sample}}}{V_{\text{vessel}}} BOD_a(\text{vessel})$$

### Special Case One-Vessel Principle

BOD<sub>a</sub> can be calculated readily from DO-data

$$\int_0^{t_{fin}} dC = \int_0^{t_{fin}} K_L a (C_e - C(t)) dt - \int_0^{t_{fin}} OURex(t) dt$$

$$C(t_{fin}) - C(0) = \int_0^{t_{fin}} K_L a (C_e - C(t)) dt - \int_0^{t_{fin}} OURex(t) dt$$

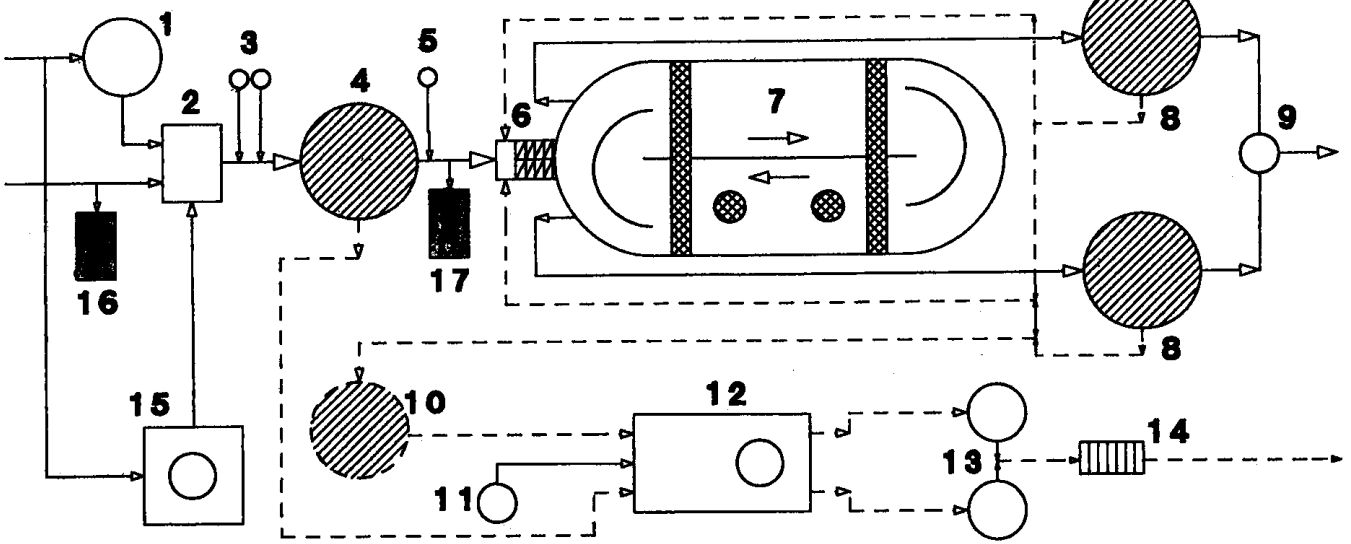
- BOD<sub>a</sub>

$$BOD_a = K_L a A$$

With this, one can eliminate K<sub>L</sub>a:

$$BOD_a^x = \frac{K_L a A^x}{K_L a A^{old}} BOD_a^{old}$$





- |                         |  |
|-------------------------|--|
| 1. COD Buffer Tank      | 10. Sludge Thickener                                 |
| 2. Equalization Basin   | 11. FeCl <sub>3</sub> /CaCO <sub>3</sub> dosing Unit |
| 3. pH Control Equipment | 12. Sludge Conditioning                              |
| 4. Primary Clarifier    | 13. Sludge Buffer Tank                               |
| 5. P-dosing Unit        | 14. Sludge Filter Press                              |
| 6. Archimedes Screws    | 15. Calamity Basin                                   |
| 7. Aeration Basin       | 16. RODTOX 1   |
| 8. Secondary Clarifier  | 17. RODTOX 2   |
| 9. Effluent Tank        |  |

## Application 1 Deussa Antwerp Industrial WWTP

### Treatment Plant Configuration

- Two Wastewater Supply Routes:**
- Highly Varying Composition
  - Constant Composition -> Buffer Tank

**Calamity Basin for Toxicity/Overload Protection**

### Respirometer Setup

**'1991: First Respirometer at Inlet Oxidation Ditch**

**Large Load Variations**

**Corresponding with Batch Productions**

**Increased Use for Off-line Analysis**

- Biodegradability Tests, Toxicity
- Production Divisions' Invoice

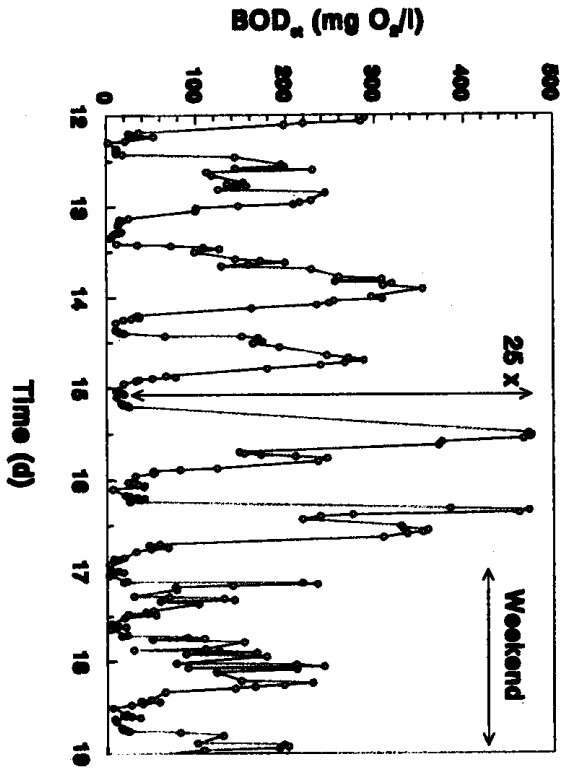
**'1993: Second Respirometer  
at Highly Varying Wastewater Stream**

### Feedforward Control Study

- Control of Buffer Tank to**
- Equalize Loads
  - Reduce Electricity Bill
- Control of Calamity Basin to Protect for Overloads**

**Application 2**  
**Maria Middelaers Hospital WWTP**

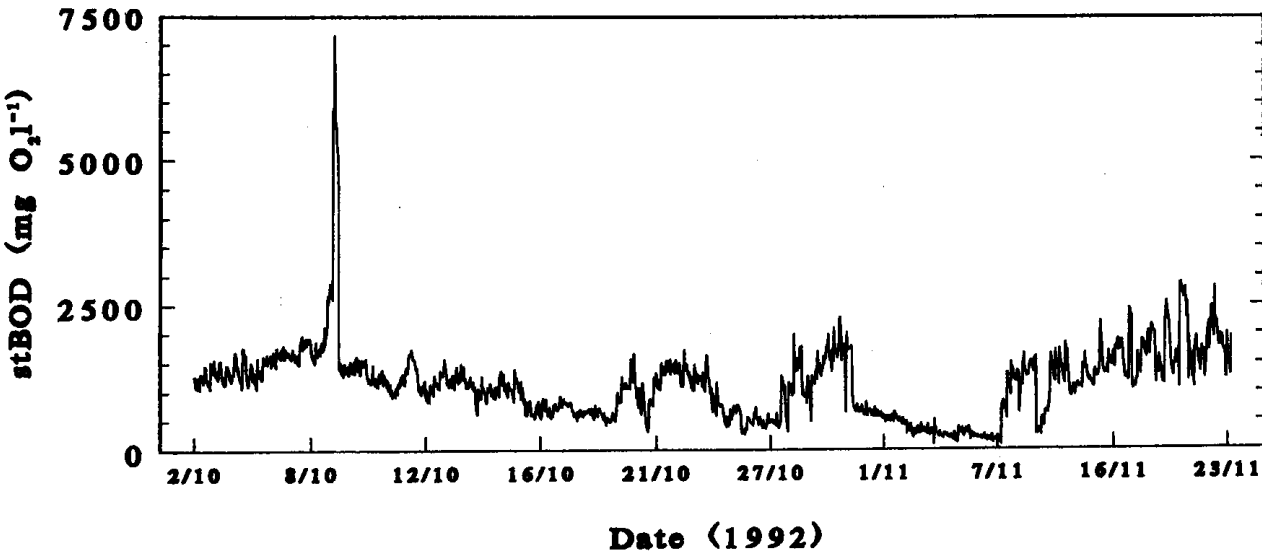
Experiment set up to Check Long-term Stability of Respirometric Devices for BOD<sub>u</sub> (see below) and Toxicity Monitoring (Kong, In Preparation)



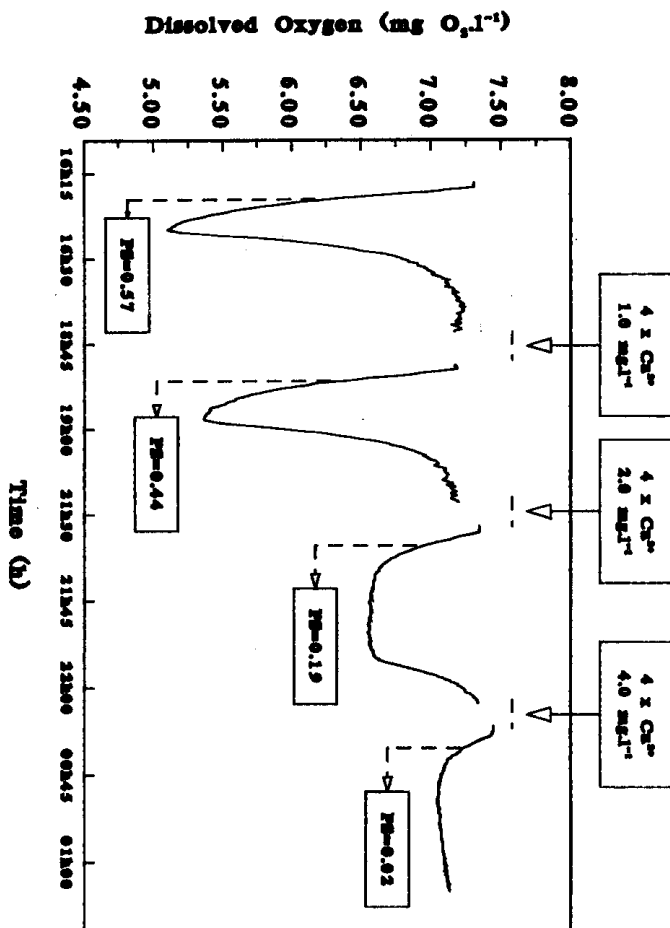
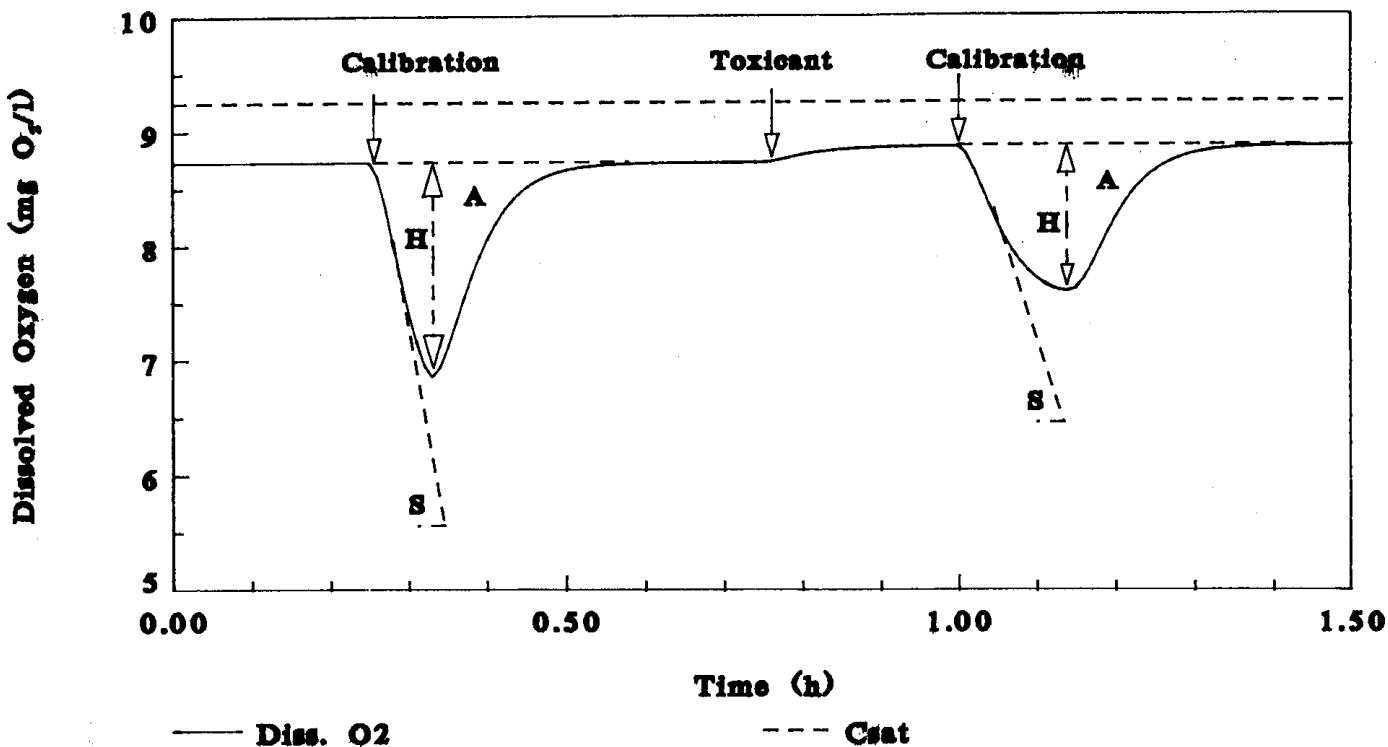
**High Loads at Day-time when Staff is Present**  
**Very Low Waste Content at Night**  
**Reduced Pollutant Load during Weekends**

**Implementations allow to Cover this BOD<sub>u</sub> Range**  
**With Buffer Tank, Load Equalization is Possible**

**ROD TOX Wastewater Load Monitoring**  
**2 months, 1800 respirograms**



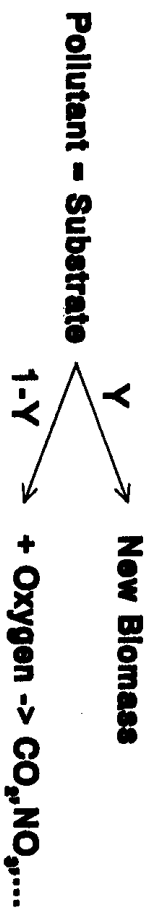
# ROD TOX TOXICITY Test PRINCIPLE



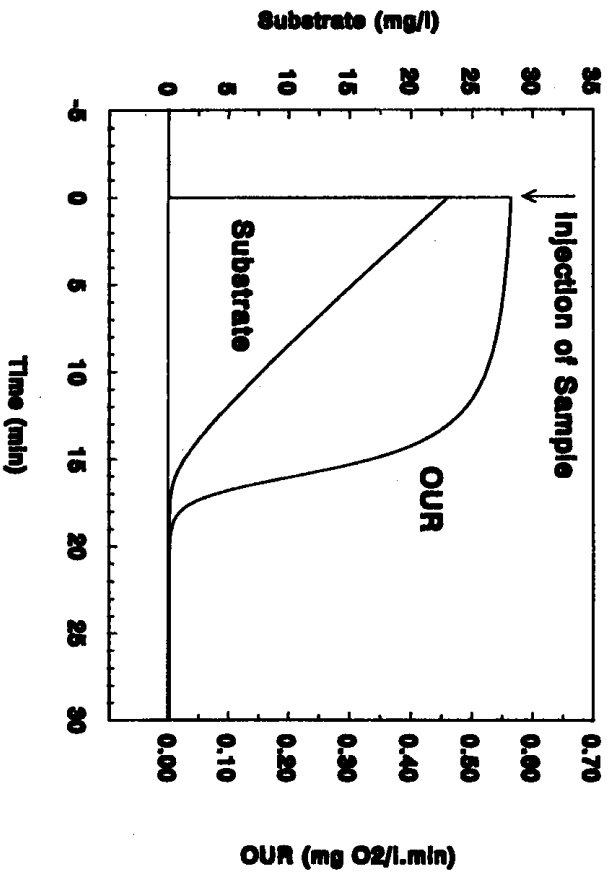
## Wastewater Copper Concentration

	0.0	1.0	2.0	4.0
PS	0.57	0.44	0.19	0.02
PH	2.20	1.81	0.80	0.38
PA	18.6	16.7	17.0	17.5
C <sub>o</sub>	7.22	7.20	7.45	7.63
Time	20.1	22.9	36.3	64.0

## Respirograms: Background



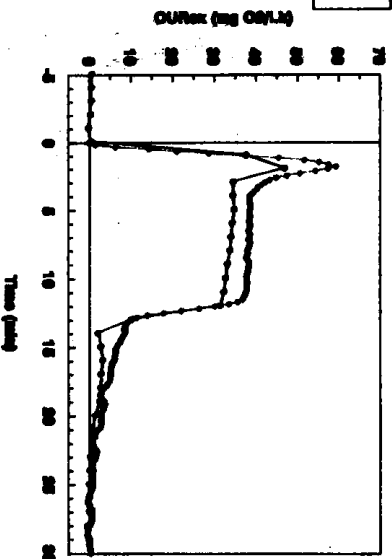
Oxygen Uptake Rate =  $(1-Y) \cdot \text{Substrate Degradation Rate}$



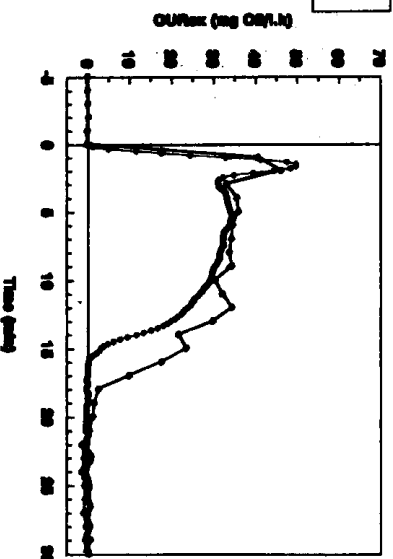
Alm: Characterize Biodegradation of Pollutants  
 via Interpretation of recorded OUR profiles

## WATER 1

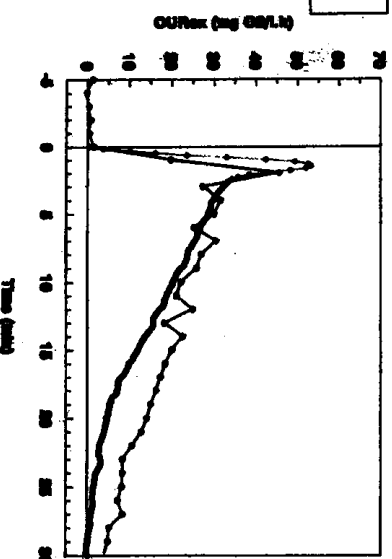
Method 1  
 Method 2



Sludge 2



Sludge 3



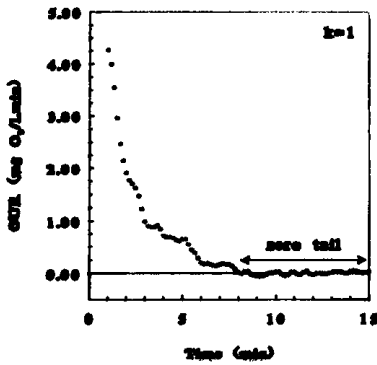
# Candidate Biodegradation Models

## Exponential

$$r_{o1} = \frac{\mu_1 X}{Y_1} S_1$$

$$\frac{dS_1}{dt} = -r_{o1}$$

$$OUR_{ex} = (1-Y_1) \cdot r_{o1}$$

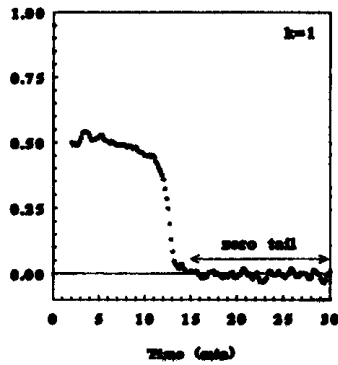


## Single Monod

$$r_{o1} = \frac{\mu_1 X S_1}{Y_1(K_{o1} + S_1)}$$

$$\frac{dS_1}{dt} = -r_{o1}$$

$$OUR_{ex} = (1-Y_1) \cdot r_{o1}$$



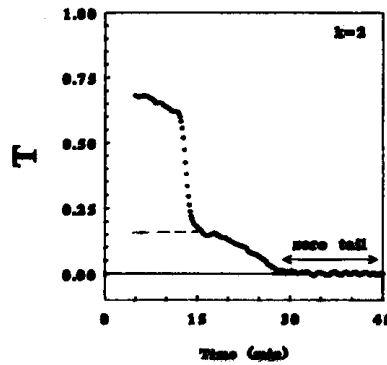
## Double Monod

$$r_{o1} = \frac{\mu_1 X S_1}{Y_1(K_{o1} + S_1)} \quad r_{o2} = \frac{\mu_2 X S_2}{Y_2(K_{o2} + S_2)}$$

$$\frac{dS_1}{dt} = -r_{o1}$$

$$\frac{dS_2}{dt} = -r_{o2}$$

$$OUR_{ex} = (1-Y_1) \cdot r_{o1} + (1-Y_2) \cdot r_{o2}$$



## Application of On-line Modelling with In-Sensor-Experiments (Kong, 1994)

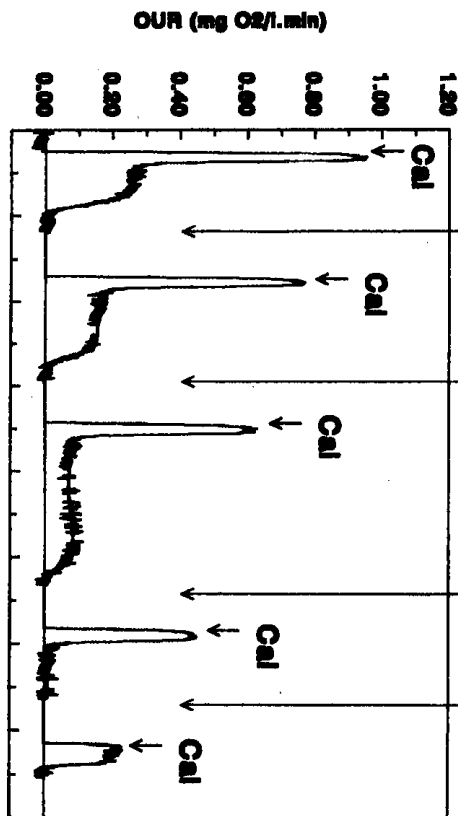
Simultaneous Characterization of :

- Aerobic Carbon-oxidation Capacity of the Sludge
- Nitrification Capacity

Principle:

Calibrate with Mixture of C-source/ $NH_4Cl$  (Double Monod)

Injections with Cyanide containing Wastewater

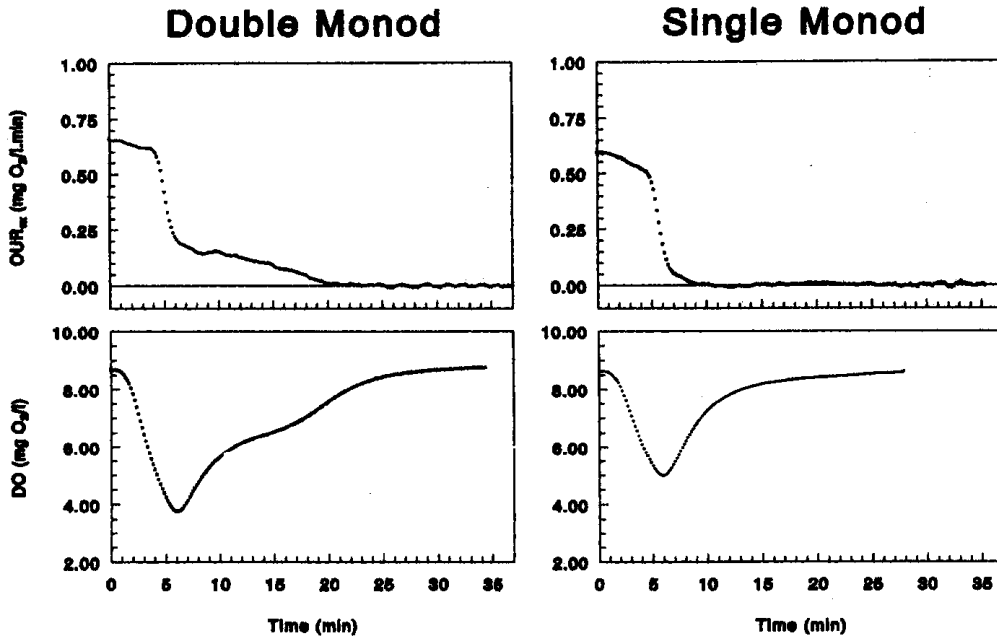


Parameter Change ( $\mu_2$  decreases)

Structure Change (Double -> Single)

# MATHEMATICAL MODELS

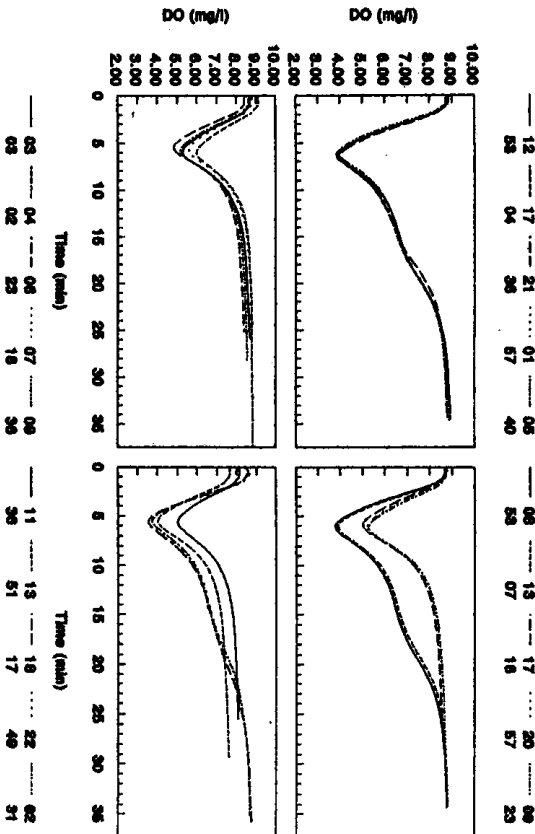
Typical Results:



## RESULTS

Toxicity Event R2 (February 17-20 1994)

Raw Data (20 respirograms)



Visual Inspection:

Toxicity detected: 18/2/94 at 17:18  
 Recovery observed: 19/2/94 at 18:17

Automation ?

On-line Model Identification

-> Parameter change  
 -> Model Structure change

Model selection

- Fit:  $MSE = J(n-p)$
- FitComplexity:  $AIC = n \cdot \log(J/n) + 2p$
- Residuals Analysis: Runs

Detection in due time ! => On-line ! => fast NPE

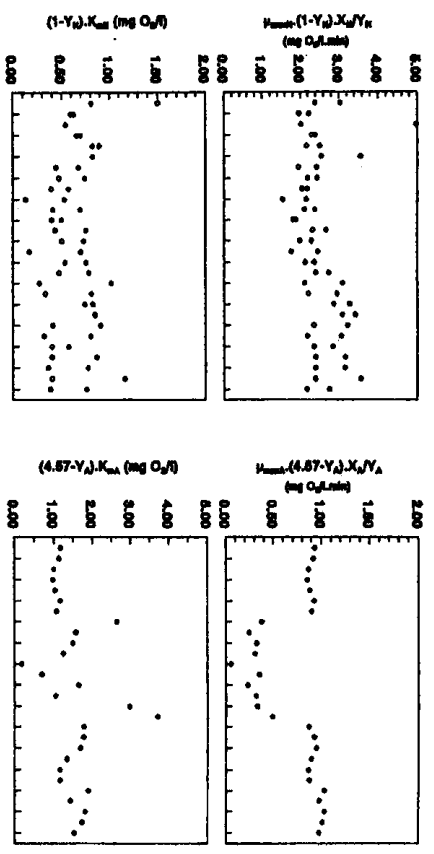
# RESULTS

(continued)

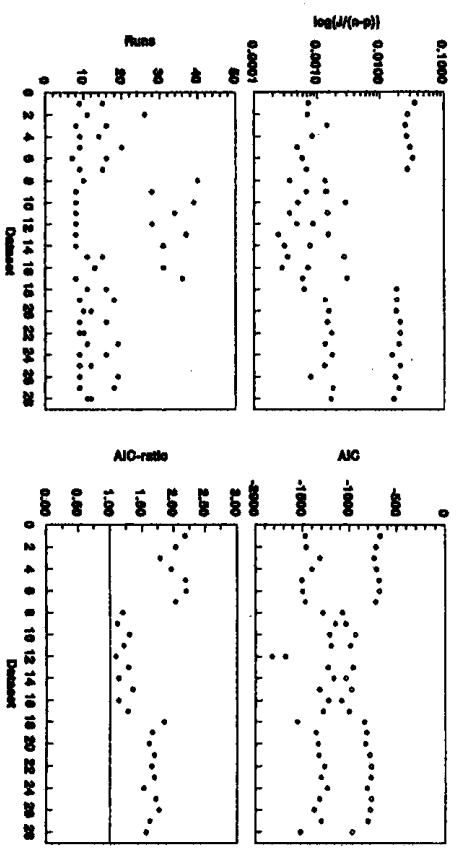
Parameters:

Heterotrophs (Acetate)

Autotrophs (ammonia)



Model Selection:

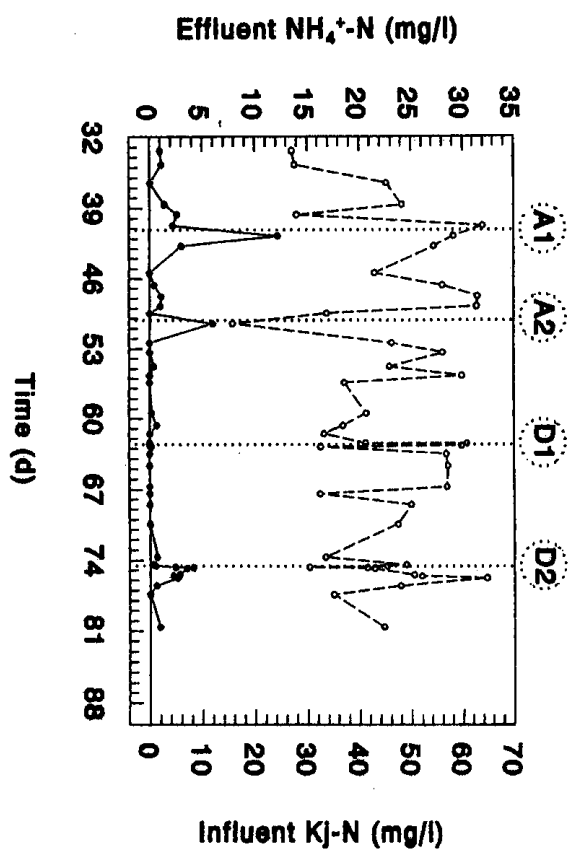


# RESULTS

Two month evaluation period:

- 2 accidental intoxications R1, R2
- 2 deliberate intoxications D1, D2

Effect on Nitrogen Oxidation:



Deliberate intoxications with creoline ( $IC_{50}=7.5$ ;  $IC_{50}=40$  ppm)

Procedure:

- D1: Creoline addition stopped after alarm => PROTECTION I
- => Concentration in Ferretion tank = 5 ppm
- D2: Addition of Creoline continued after toxicity alarm
- => Concentration in Ferretion tank = 25 ppm
- => Effluent ammonia increases to 5 ppm