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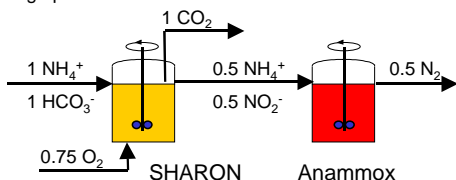
## Introduction

### The SHARON-Anammox process

The combined SHARON-Anammox process is a promising process for biological nitrogen removal from ammonium-rich wastewater (~1gNH<sub>4</sub>-N/l).

Advantages compared to conventional nitrification-denitrification:

- savings on aeration energy (63%)
- no need for carbon source addition
- low sludge production



The optimal nitrite/ammonium ratio (1/1 in theory) in the Anammox influent should be produced by the SHARON process.

### The SHARON process

- completely stirred tank reactor (CSTR)
  - high temperature (~35°C)
  - short retention time (~1day)
  - protons produced during nitrification are neutralized through CO<sub>2</sub> stripping
- In theory:

$$\text{IF } \left( \frac{\text{HCO}_3^-}{\text{NH}_4^+} \right)_{\text{influent}} = \frac{1}{1} \quad \text{THEN } \left( \frac{\text{NO}_2^-}{\text{NH}_4^+} \right)_{\text{produced}} = \frac{1}{1}$$

In practice:

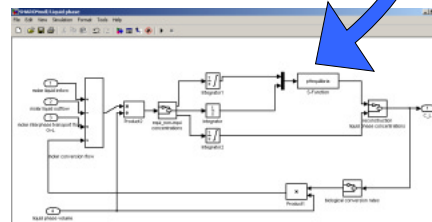
The produced nitrite/ammonium ratio is influenced by a number of factors.

## The SHARON model

Implemented in Matlab 6.1-Simulink 4.1

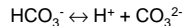
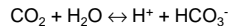
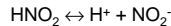
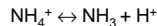
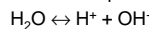
Consists of

- 16 liquid phase mass balances
- 5 biological conversion processes in liquid phase
- 3 gas phase mass balances
- diffusion processes between gas and liquid phase

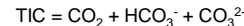
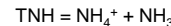


pH effects are very important ⇒

chemical equilibria are considered & lumped components are defined:



assume steady state



From the charge balance in the reactor:



the pH and corresponding equilibrium concentrations are calculated.

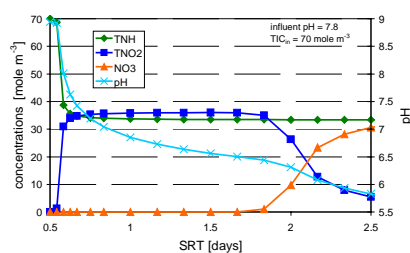
## Objective

Perform a simulation study to examine the influence of operating parameters on the nitrite/ammonium ratio produced by the continuously aerated SHARON process

## Simulation results

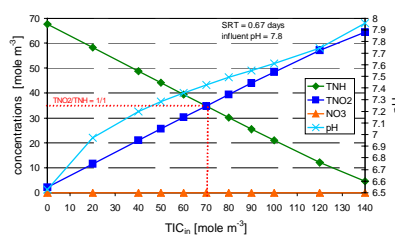
Steady state simulation results for the behaviour of the continuously aerated SHARON system are presented (influent TNH = 70 mole m<sup>-3</sup>).

### Influence of the sludge retention time



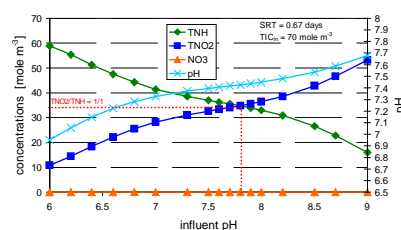
0.65 d<sup>-1</sup> < SRT < 1.6 d<sup>-1</sup> to establish partial nitrification  
 resulting  $\frac{\text{TNO}_2}{\text{TNH}}$  is hardly influenced  
 in this operating region

### Influence of the influent TIC concentration



influent TIC ↑ ⇒ HCO<sub>3</sub><sup>-</sup> ↑ ⇒  
 buffer capacity ↑ ⇒  $\frac{\text{TNO}_2}{\text{TNH}}$  ↑

### Influence of the influent pH



influent pH ↑ ⇒  $\frac{\text{HCO}_3^-}{\text{TIC}}$  ↑ ⇒  
 buffer capacity ↑ ⇒  $\frac{\text{TNO}_2}{\text{TNH}}$  ↑

## Conclusions

The  $\frac{\text{TNO}_2}{\text{TNH}}$  ratio produced by the SHARON process hardly varies with varying SRT, but is highly influenced by the buffer capacity of the influent, that varies with influent pH and TIC concentration.

## TAKE HOME MESSAGE

- For efficient realization of the combined SHARON-Anammox system, it is crucial to control the  $\frac{\text{TNO}_2}{\text{TNH}}$  ratio produced by the SHARON process
- Operating parameters influencing the buffer capacity of the SHARON system are suitable control handles