

Model-based scenario analysis of activated sludge treatment options:

Optimal but robust nutrient removal in SBRs

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- Introduction
- Systematic optimisation protocol
- Evaluation of the protocol
 - Definition of objective(s)
 - Framework of the optimisation
 - Model selection and calibration
 - Scenario analysis
 - Evaluation of the scenario analysis
- Limitations of the model-based optimisation
- Conclusions & perspectives

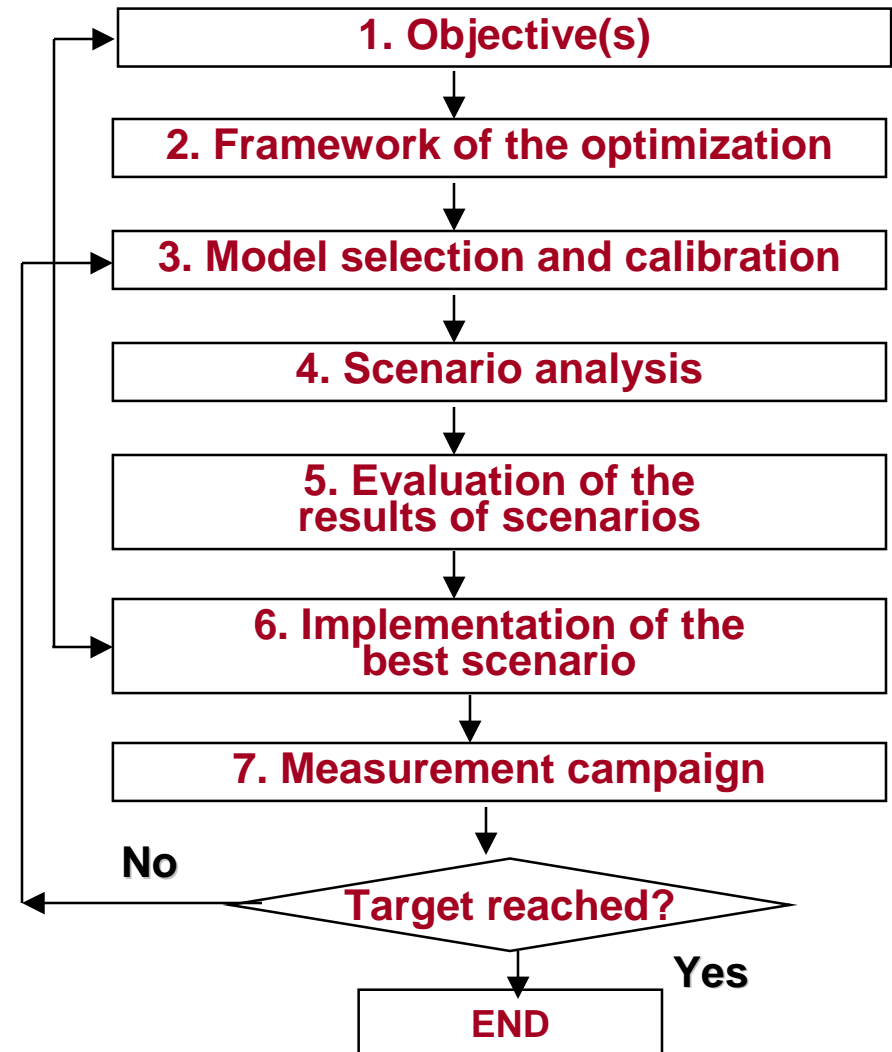
- Both N & P removal successfully demonstrated at lab- and full-scale SBR installations.
- SBR offers more flexibility in operation (compared to continuous systems) – a key aspect in process optimisation.
- Many possible operating strategies to optimise nutrient removal performance in SBRs.
- Usually process developed at lab- or pilot-scale & only comparison of a few operating scenarios
- Increasingly, mathematical models are used to search for the optimal operating scenario (e.g. ASM1 for N-removal and ASM2d for N- & P- removal)

Statement of Objective

- Systematize and standardize the model-based optimisation of SBRs. Important:
 - i. to ensure an objective and detailed search for an optimal operating strategy
 - ii. for internal quality check
 - iii. to compare different optimisation studies

Systematic optimisation protocol

- Objective oriented & iterative protocol
- A grid of scenarios (full-factorial design) built on the basis of the degrees of freedom and the constraints of the SBR system
- Selection and calibration of a suitable model to describe the biological processes
- Simulation and evaluation of a multitude of scenarios
- Selection of the best scenario
- Implementation & final evaluation



Evaluation of the systematic protocol

1. Objective

- Improved and robust N and P removal in a nutrient removing SBR

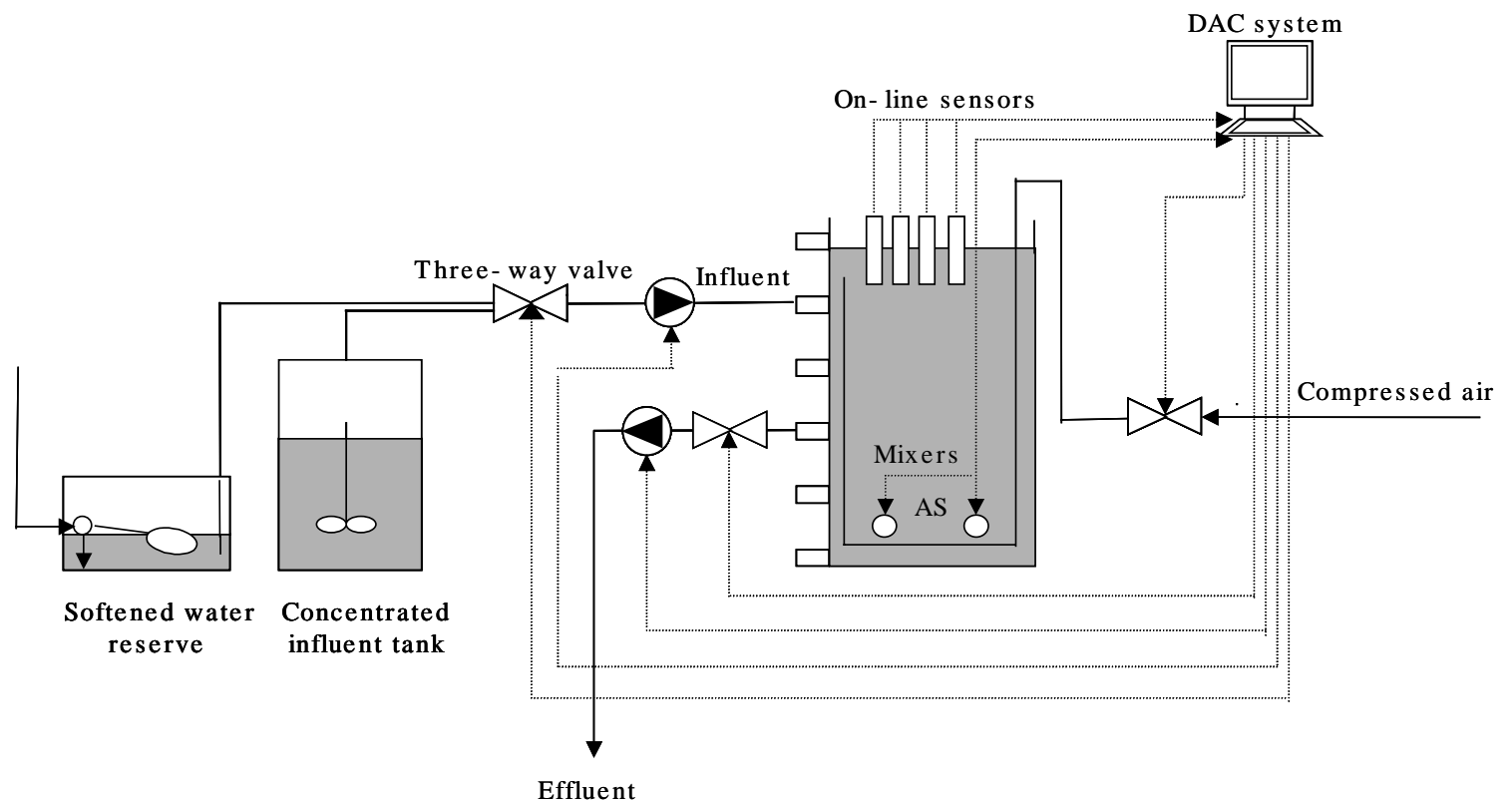
2. Framework of the optimisation

- *The SBR system:*
 - A lab-scale reactor with 80 L treating a synthetic wastewater



2. Framework of the optimisation *cont'd.*

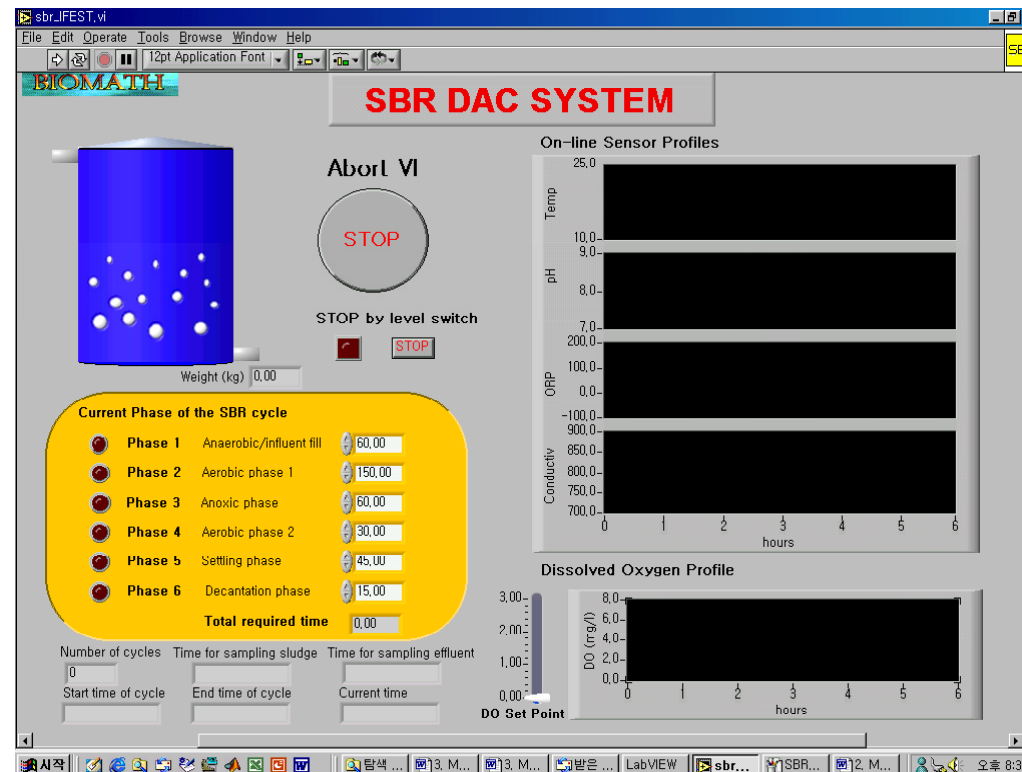
- *The SBR system:*
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2. Framework of the optimisation *cont'd.*

- *The SBR system:*
 - A lab-scale reactor with 80 L treating a synthetic wastewater

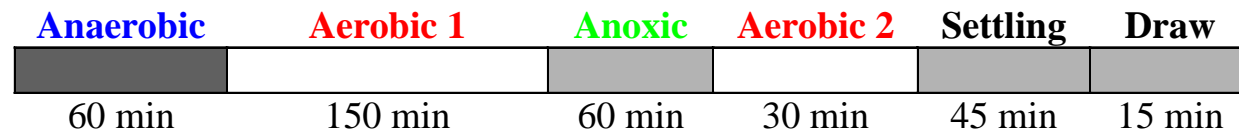
LABVIEW Data-acquisition and Control



2. Framework of the optimisation *cont'd.*

○ *Characteristics*

- $V = 80$ l
- $SRT = 10$ d, $HRT = 12$ h
- synthetic influent (COD/N/P = 100/13,7/2,14)
similar to municipal wastewater
- 4 cycles per day (6 hours)



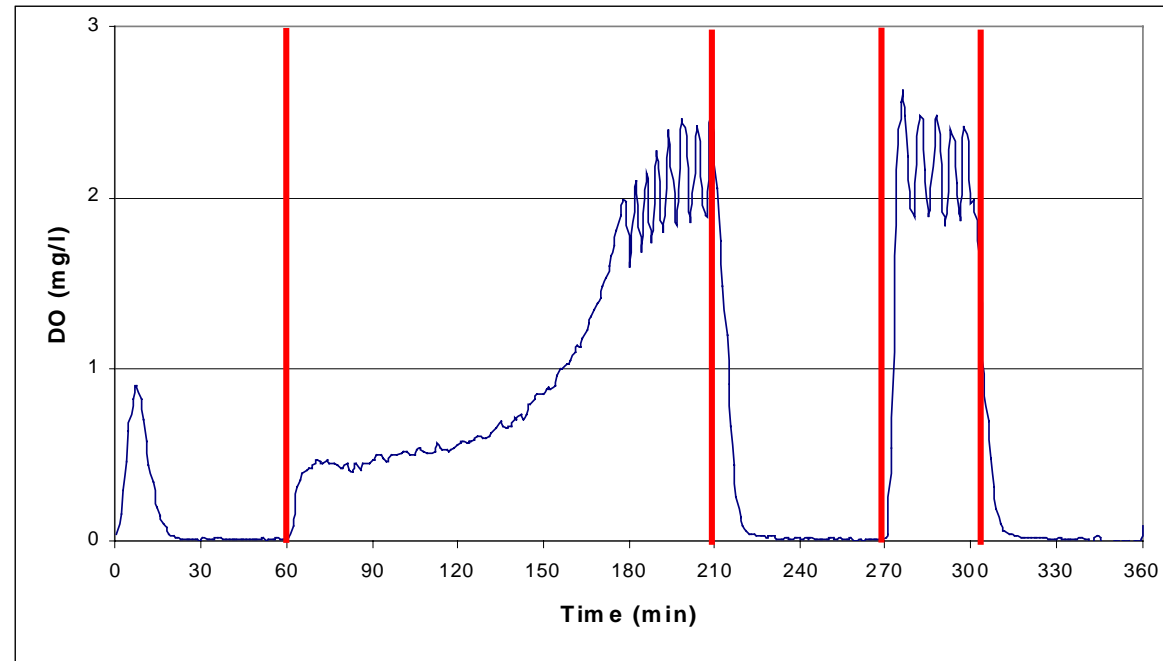
○ *Measurements*

- DO, pH, ORP, conductivity, weight (on-line - minute)
- COD, COD_{sol}, Total-N, NH₄, NO₃, NO₂, PO₄ (off-line - daily)
- MLSS (2-3 g/l), SVI (80-120 ml/g) (off-line - daily)
- DGGE (microbial community) (off-line - weekly)

2. Framework of the optimisation *cont'd*

- *The SBR system: Typical process data*

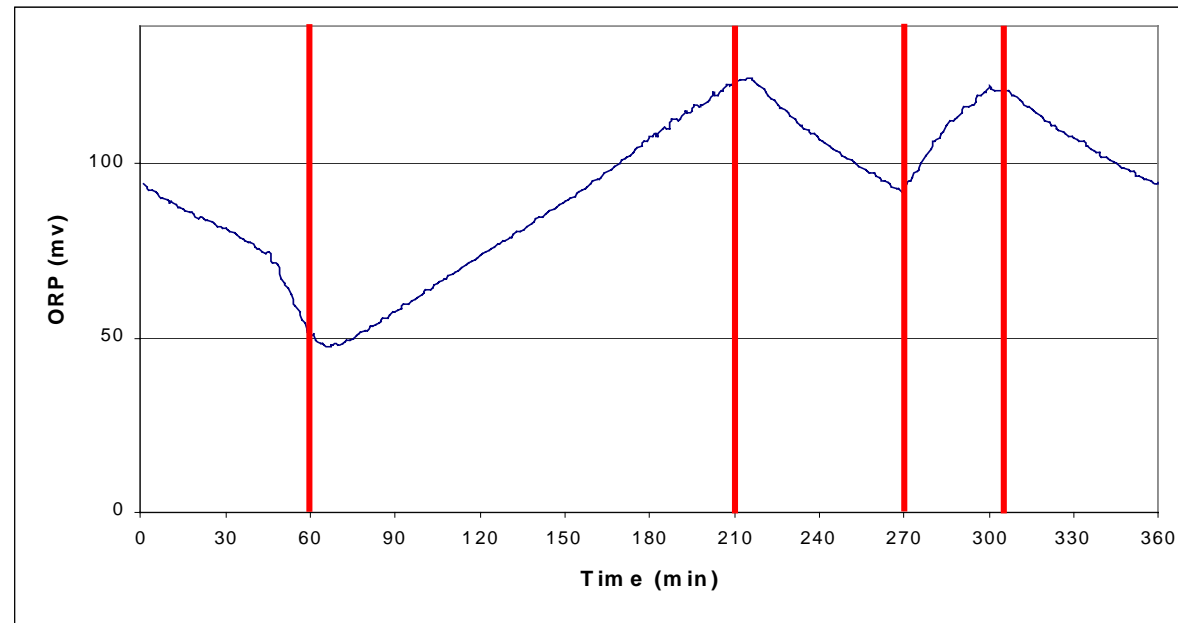
Dissolved oxygen



2. Framework of the optimisation *cont'd*

- *The SBR system: Typical process data*

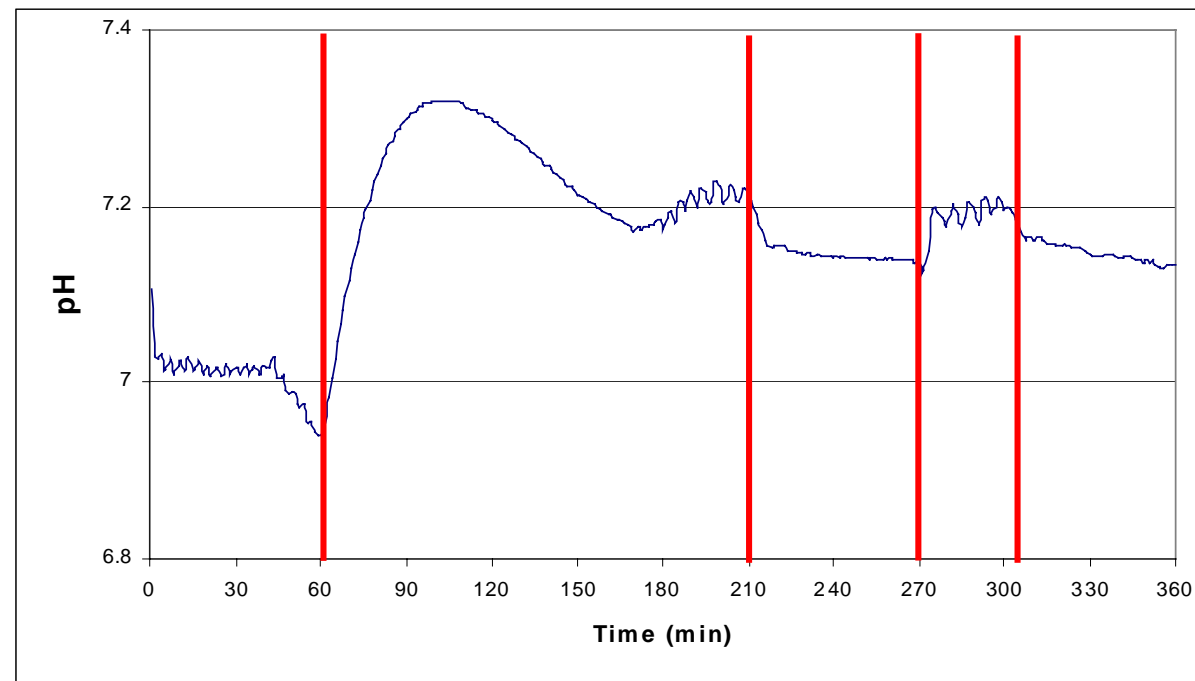
Redox potential (aeration +, denitrification -)



2. Framework of the optimisation *cont'd*

- *The SBR system: Typical process data*

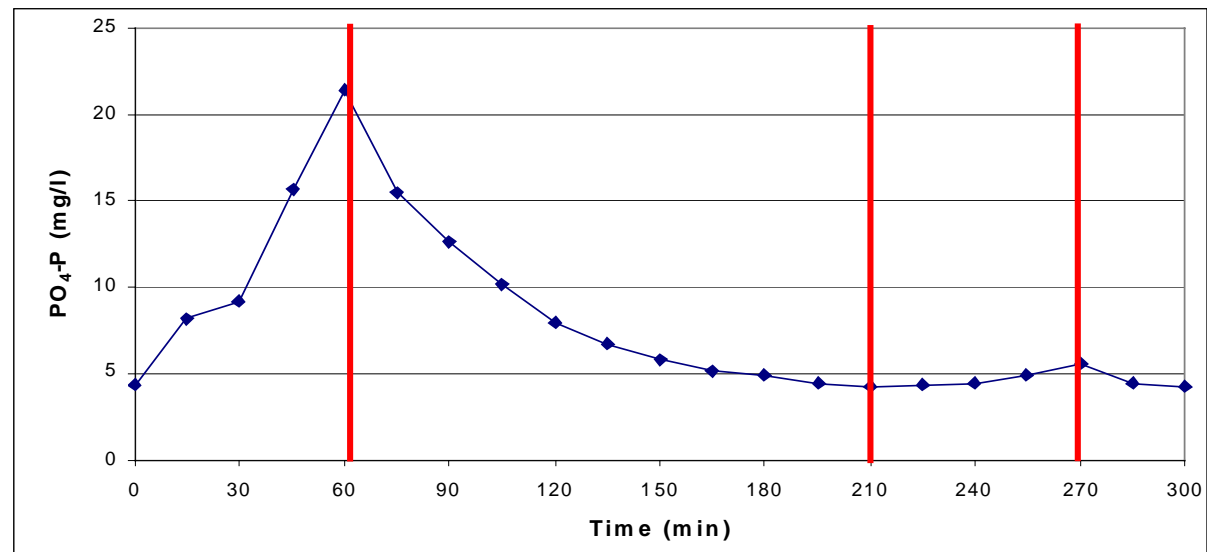
pH



2. Framework of the optimisation *cont'd*

- *The SBR system: Typical process data*

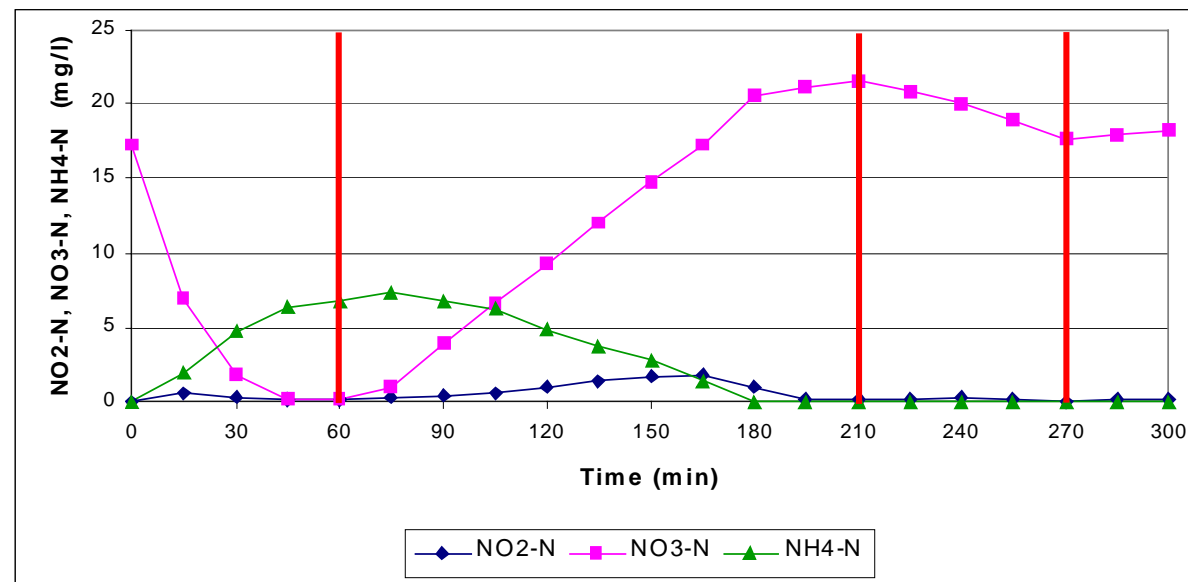
Phosphate



2. Framework of the optimisation *cont'd*

- *The SBR system: Typical process data*

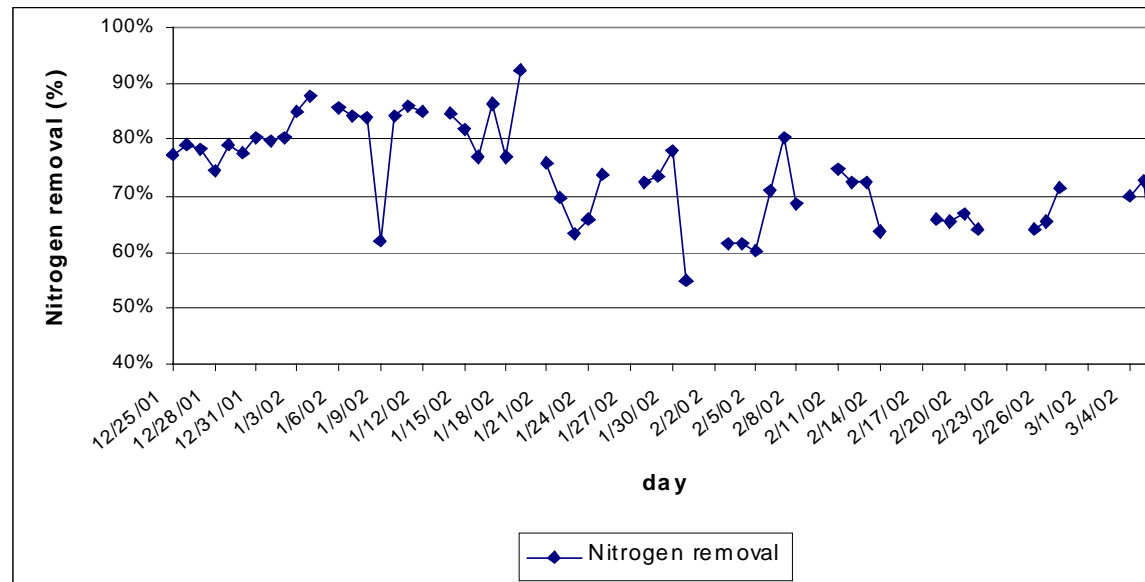
Nitrogen fractions (NH_4 , NO_3 , NO_2)



2. Framework of the optimisation *cont'd.*

○ *Performance:*

- 95 % COD-removal
- 65 % N-removal
- complete nitrification / incomplete denitrification
- 65 % PO₄-removal (limited because of nitrate presence)



2. Framework of the optimisation *cont'd.*

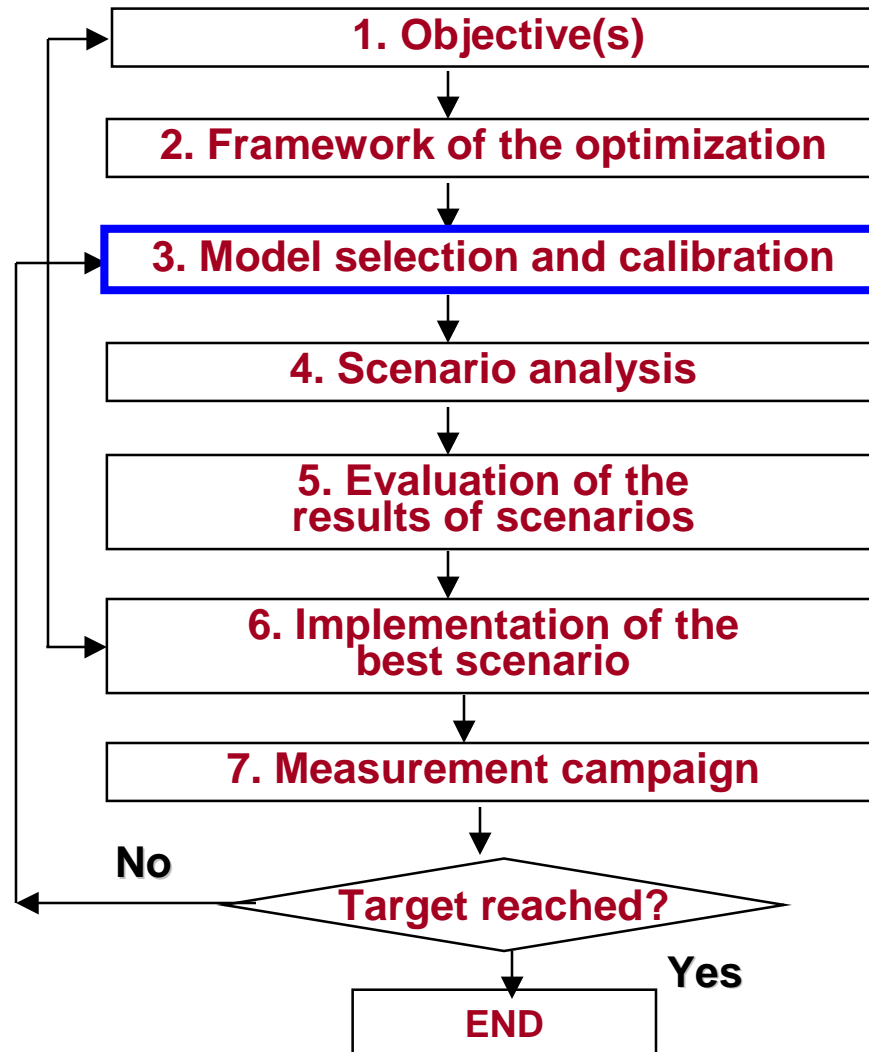
- *The SBR system:*
 1. A lab-scale reactor with 80 L treating a synthetic wastewater
- *Degrees of freedom (based on systems-analysis)*
 1. Oxygen set-point (S_O -sp)
 2. Length of the anaerobic phase (T_{ANB})
 3. Length of the reaction (aerobic + anoxic) (T_R),
 4. Step-feed of the influent to anoxic periods ($V_{\text{step-feed}}$)
 5. Intermittent aeration frequency during the react phase
i.e. more than 1 aerobic/anoxic phase per SBR cycle of 6 hours

2. Framework of the optimisation *cont'd.*

- *Constraints*

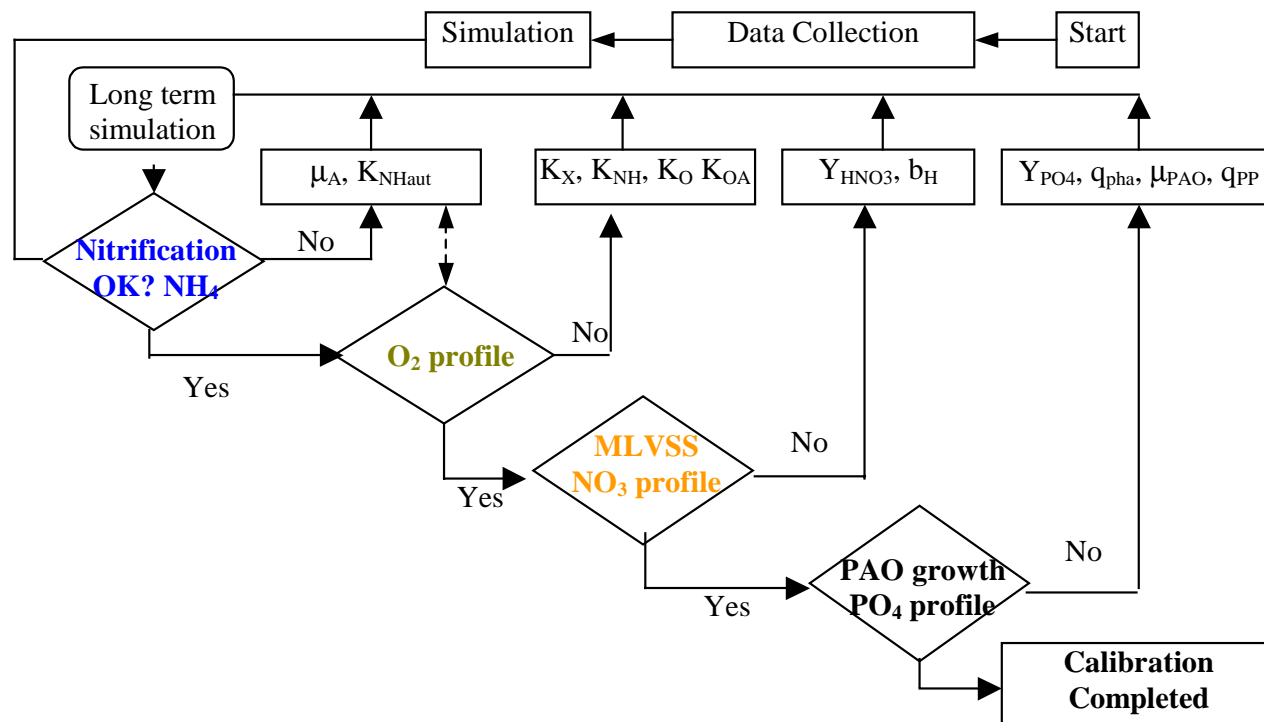
1. Total volume (80 L)
2. The volumetric exchange ratio, $V_{\text{initial}}/V_{\text{total}}$ (0.5)
3. SRT (10 d) & HRT (12 h)
4. The total cycle length (360 min)
5. The $K_L a$ is sufficiently high *to ensure oxygen at set-point value*
6. The settling/draw phase fixed (60 min)

Systematic optimisation protocol



3. Model selection and calibration

- *Selected model:*
ASM2d extended with hydrolysis of organic nitrogen module of ASM1
- *Systematic calibration procedure:*

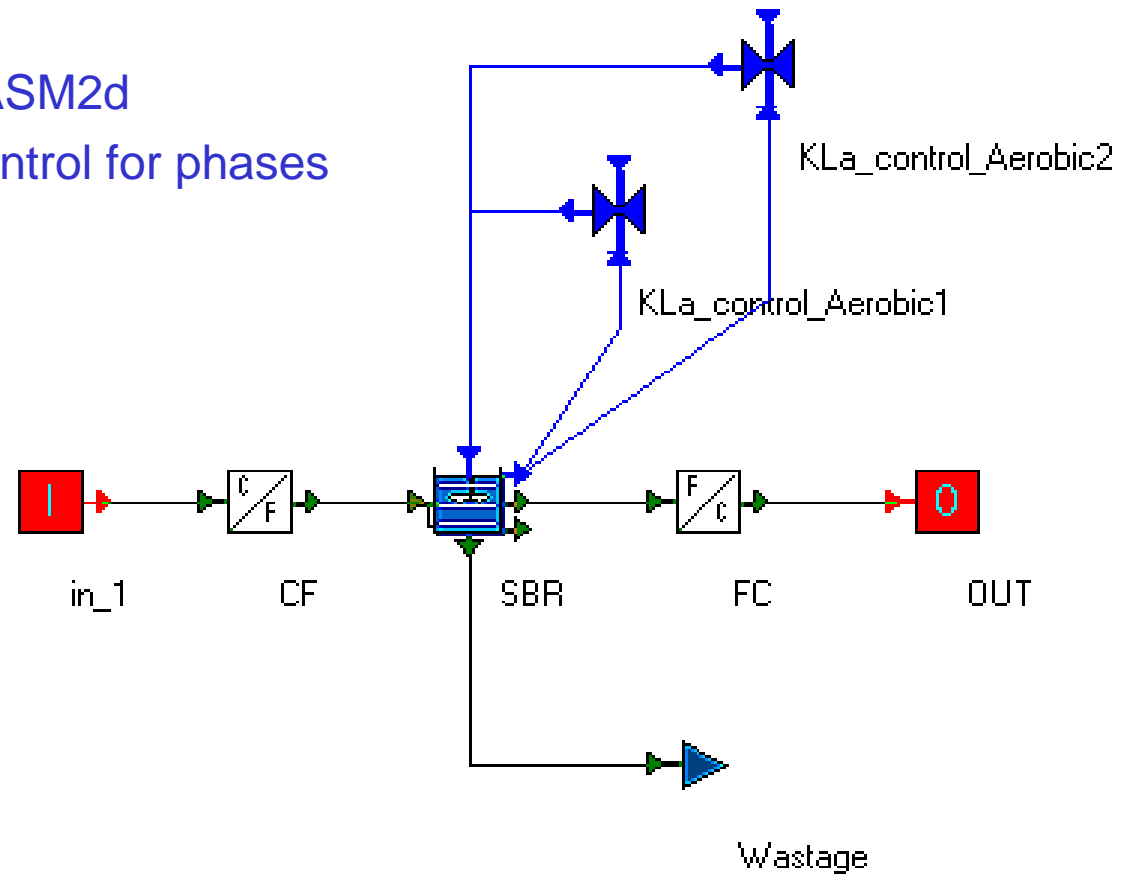


3. Model selection and calibration

○ *Model implementation:*

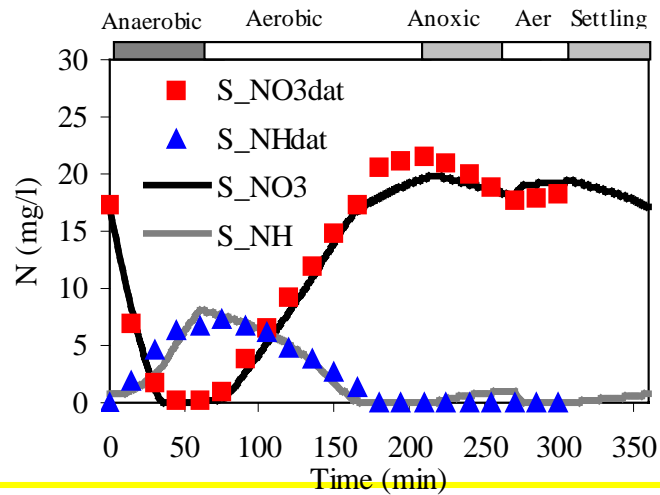
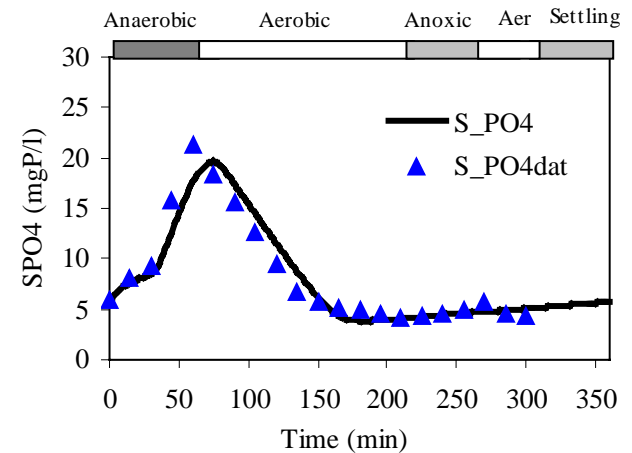
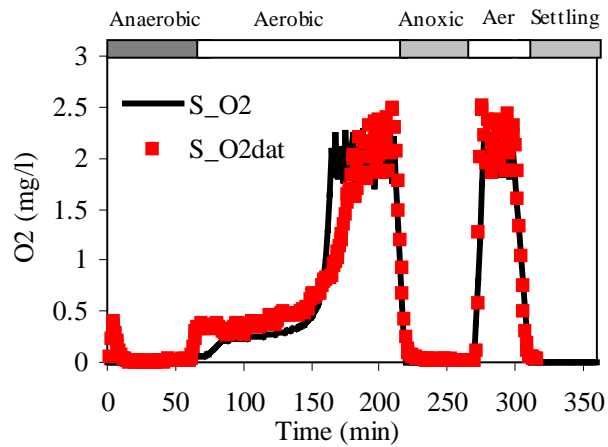
in WEST[®] with

- extended ASM2d
- aeration control for phases



3. Model selection and calibration *cont'd.*

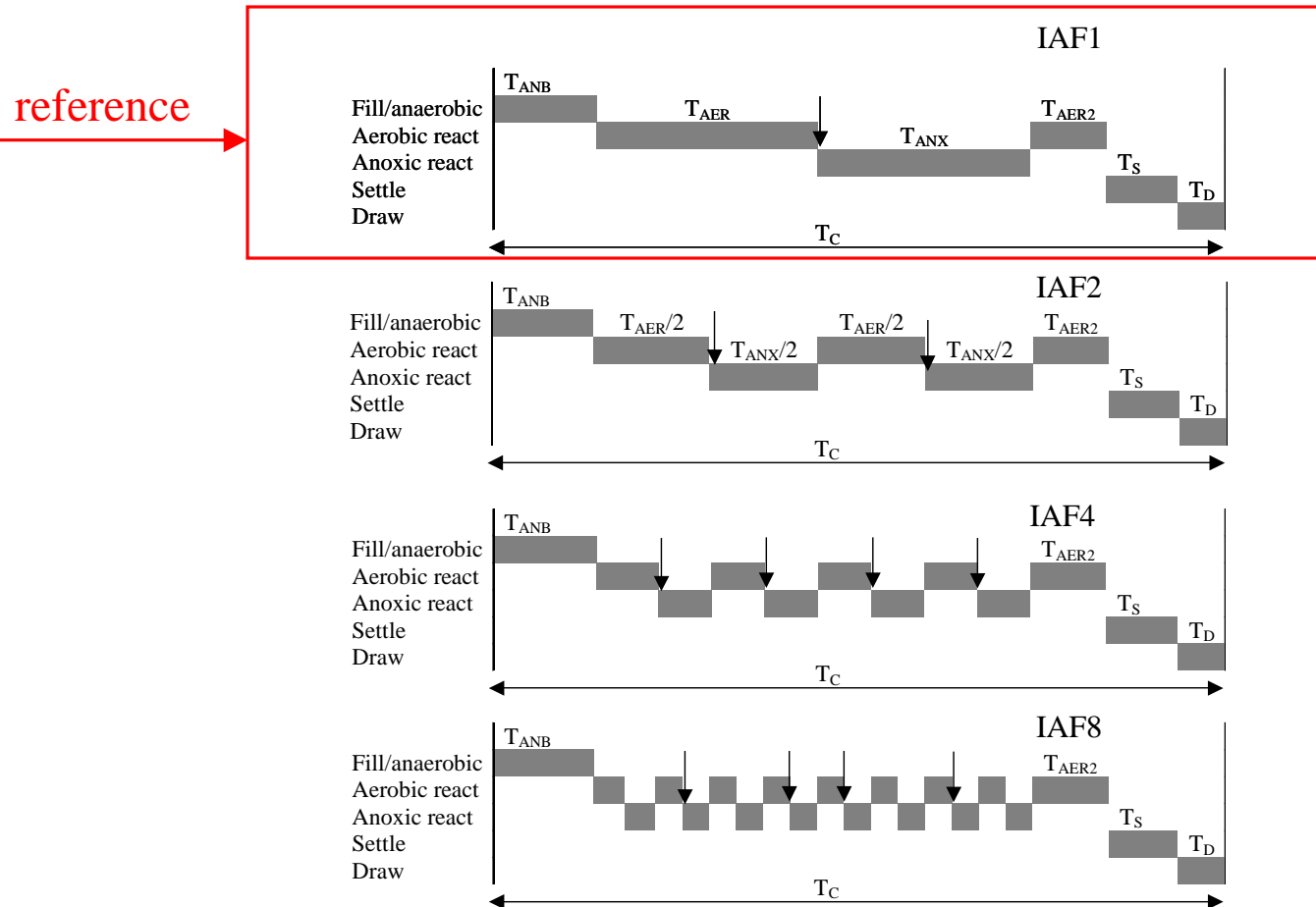
○ Calibration results:



4. Scenario analysis

- Formulation of grids of scenarios:

Configuration of intermittent aeration frequencies & step-feed of influent (↓)

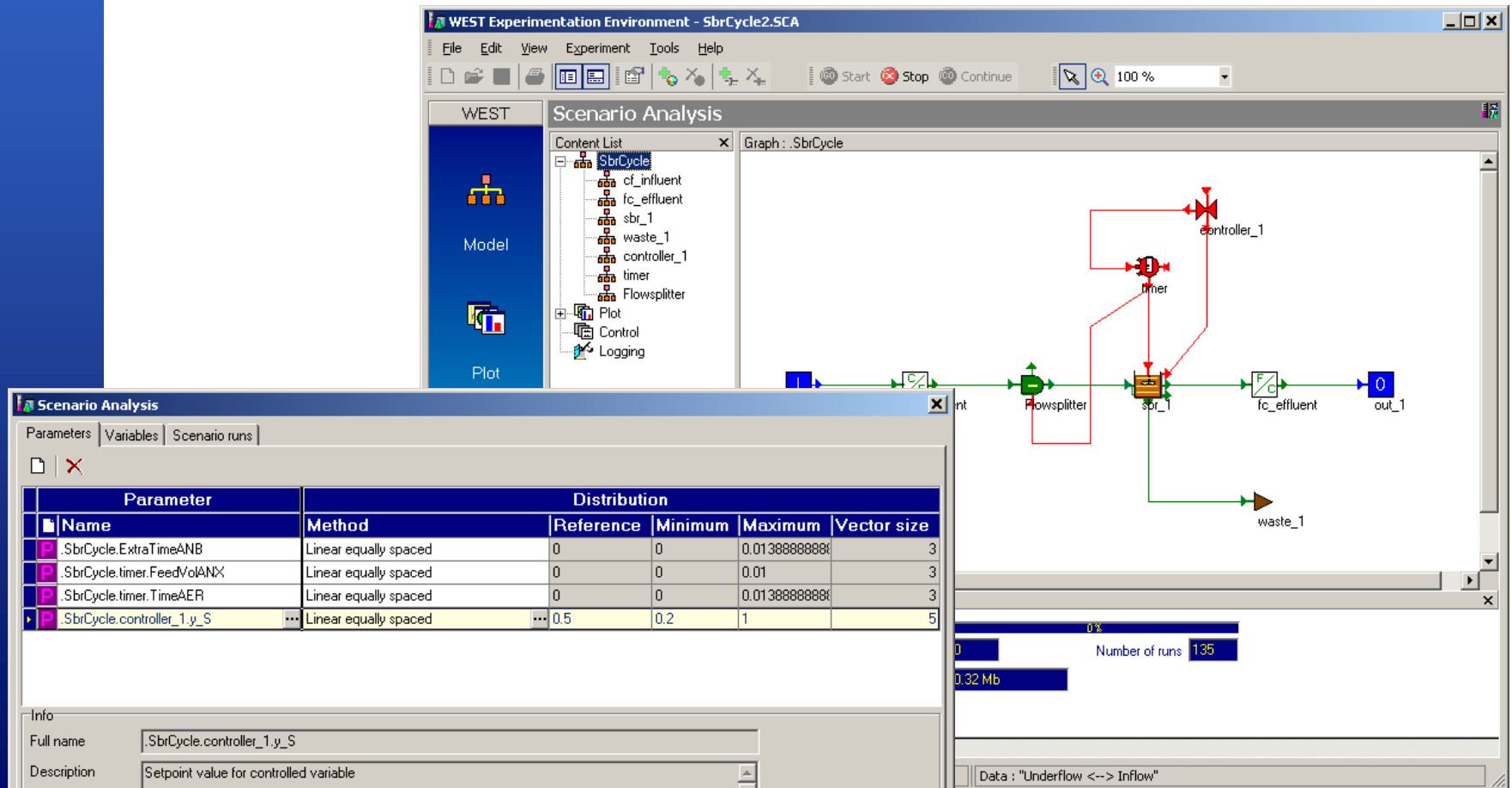


4. Scenario analysis *cont'd.*

- Construction of grids of scenarios
 - Choose a range and interval for the degrees of freedoms
 - S_{O-sp} : [0.2, 0.4, 0.6, 0.8, 1.0]
 - $V_{step-feed}$: [0, 5, 10]
 - T_{ANB} : [60, 70, 80]
 - T_{AER} : [130, 140, 150]
 - Intermittent aeration frequency:[1, 2, 4, 8]
 - Full-factorial design of degrees of freedoms:
 - ➔ total 648 scenarios
 - Simulate each scenario for 3 X SRT, in this case 30 days

4. Scenario analysis cont'd.

- WEST Scenario analysis tool



The screenshot shows the WEST Experimentation Environment interface for 'SbrCycle2.SCA'. The main window displays a process flow diagram with components like 'timer', 'controller_1', 'sbr_1', 'flow splitter', 'fc_effluent', and 'waste_1'. A 'Scenario Analysis' dialog box is open in the foreground, showing a table of parameters and their distributions.

Parameter		Distribution			
Name	Method	Reference	Minimum	Maximum	Vector size
.SbrCycle.ExtraTimeANB	Linear equally spaced	0	0	0.013888888888888888	3
.SbrCycle.timer.FeedVolANX	Linear equally spaced	0	0	0.01	3
.SbrCycle.timer.TimeAER	Linear equally spaced	0	0	0.013888888888888888	3
.SbrCycle.controller_1.y_S	Linear equally spaced	0.5	0.2	1	5

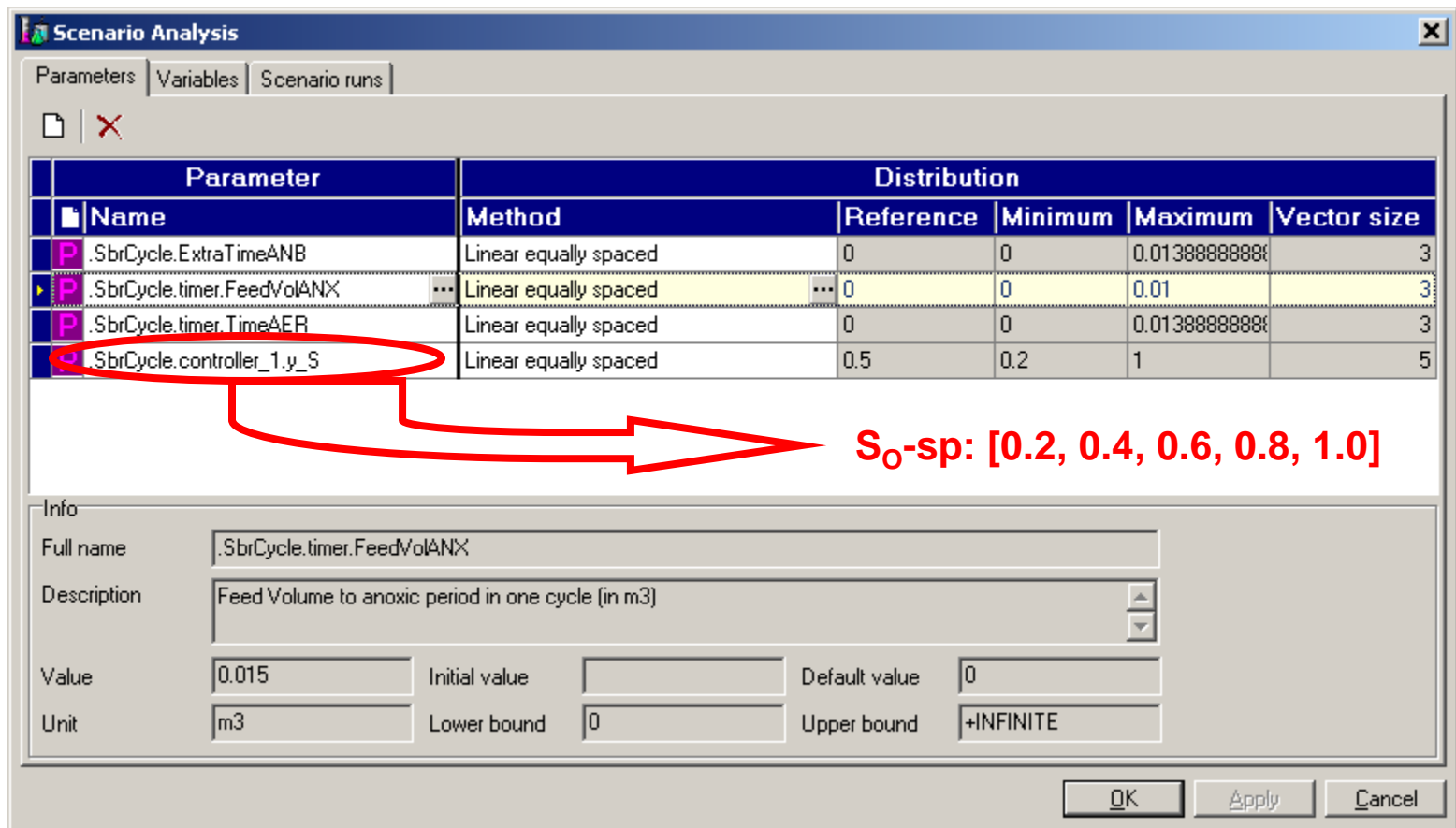
Info:
Full name: .SbrCycle.controller_1.y_S
Description: Setpoint value for controlled variable

Number of runs: 135
0.32 Mb

Data: "Underflow <--> Inflow"

4. Scenario analysis *cont'd.*

- WEST Scenario analysis tool: Scenario generator



The screenshot shows the 'Scenario Analysis' dialog box with the 'Parameters' tab selected. The main table lists parameters and their distributions:

Parameter		Distribution			
Name	Method	Reference	Minimum	Maximum	Vector size
.SbrCycle.ExtraTimeANB	Linear equally spaced	0	0	0.013888888888888888	3
.SbrCycle.timer.FeedVolANX	Linear equally spaced	0	0	0.01	3
.SbrCycle.timer.TimeAER	Linear equally spaced	0	0	0.013888888888888888	3
.SbrCycle.controller_1.y_S	Linear equally spaced	0.5	0.2	1	5

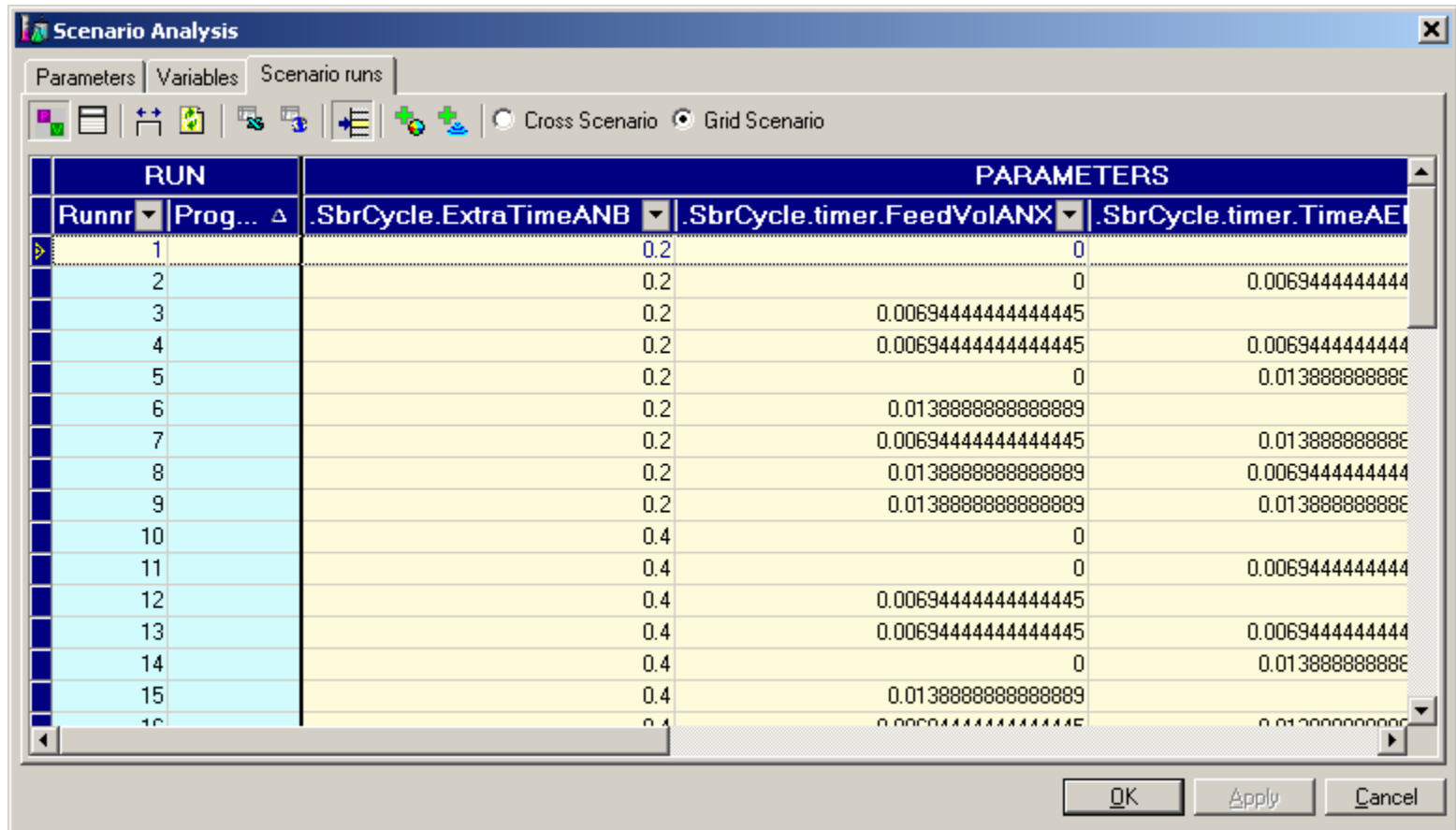
A red circle highlights the parameter '.SbrCycle.controller_1.y_S'. A red arrow points from this circle to the text **S_O-sp: [0.2, 0.4, 0.6, 0.8, 1.0]**.

The 'Info' section at the bottom shows details for the selected parameter:

- Full name: .SbrCycle.timer.FeedVolANX
- Description: Feed Volume to anoxic period in one cycle (in m3)
- Value: 0.015
- Unit: m3
- Initial value: (empty)
- Lower bound: 0
- Default value: 0
- Upper bound: +INFINITE

4. Scenario analysis *cont'd.*

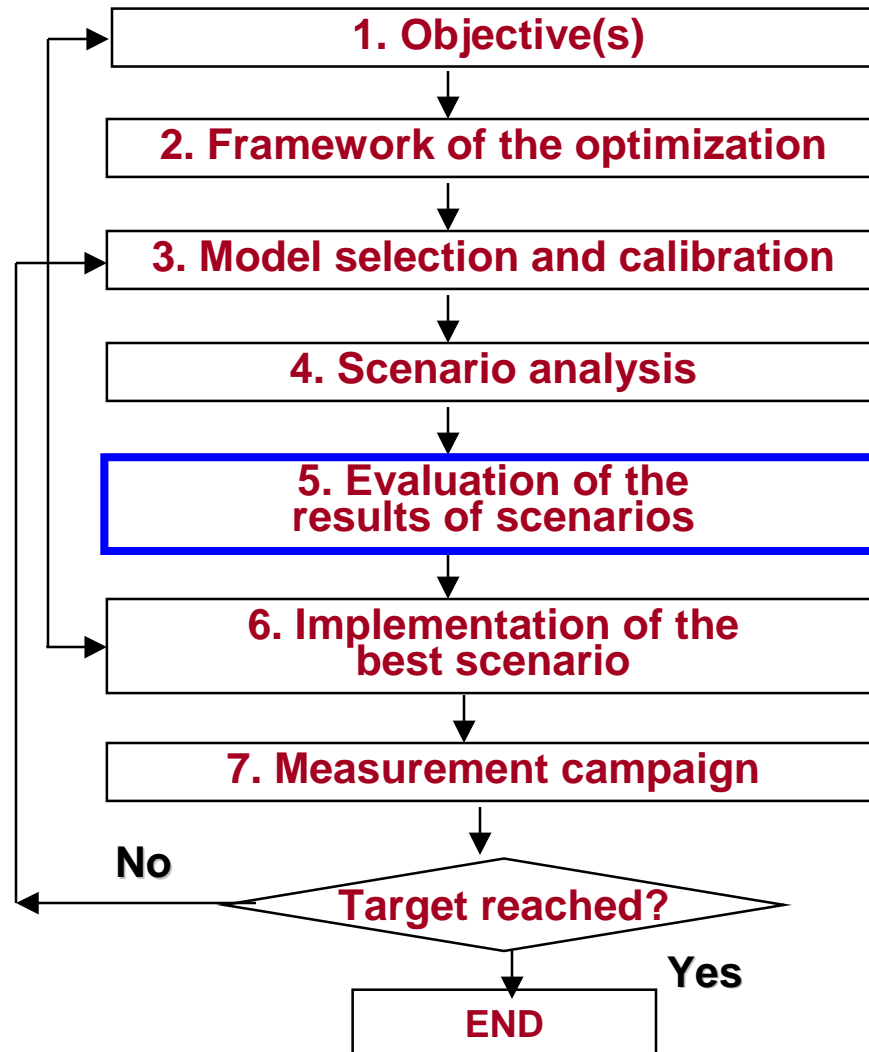
- WEST Scenario analysis tool: Scenario results window



The screenshot shows the 'Scenario Analysis' window with the 'Scenario runs' tab selected. The window contains a table with columns for 'RUN' (Runnr, Prog...), and 'PARAMETERS' (.SbrCycle.ExtraTimeANB, .SbrCycle.timer.FeedVolANX, .SbrCycle.timer.TimeAE). The table lists 16 runs with varying parameter values.

RUN	PARAMETERS
Runnr	.SbrCycle.ExtraTimeANB
1	0.2
2	0.2
3	0.2
4	0.2
5	0.2
6	0.2
7	0.2
8	0.2
9	0.2
10	0.4
11	0.4
12	0.4
13	0.4
14	0.4
15	0.4
16	0.4

Systematic optimisation protocol



5. Evaluation of the scenarios

○ Effluent quality

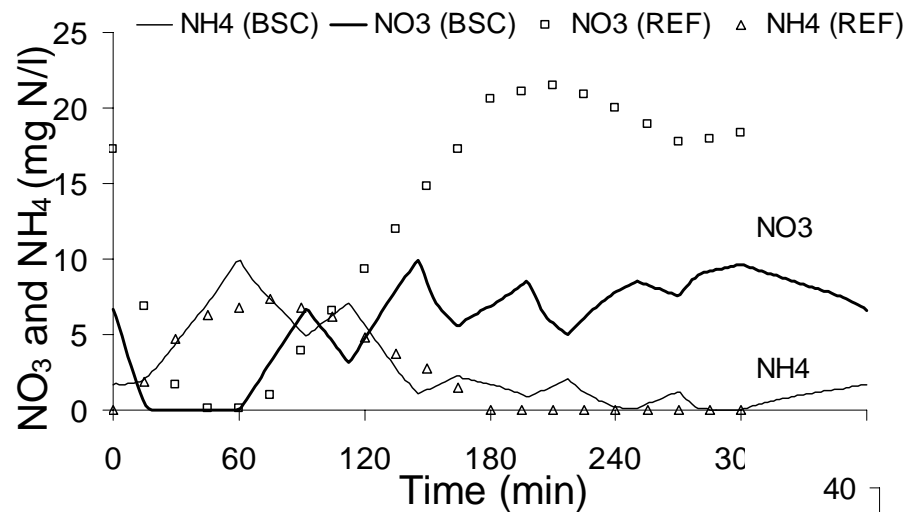
Effluent quality of 648 scenarios were analysed

Conclusions:

- Increasing T_{ANB} improves P-removal but decreases N-removal
- Increasing T_{AER} slightly improves the nitrification but negative effect on denitrification.
- The S_O -sp is the most critical/dictates the overall behaviour of the system.
- The step-feed has a positive effect on the denitrification.
- Increasing the intermittent aeration frequency (IAF) increases N & P removal

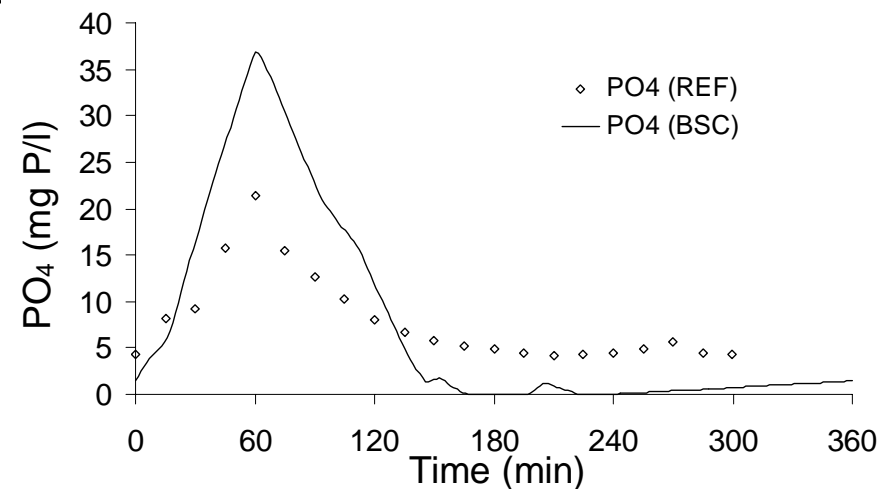
5. Evaluation of the scenarios *cont'd.*

- Simulation of best scenario: 4 aeration phases

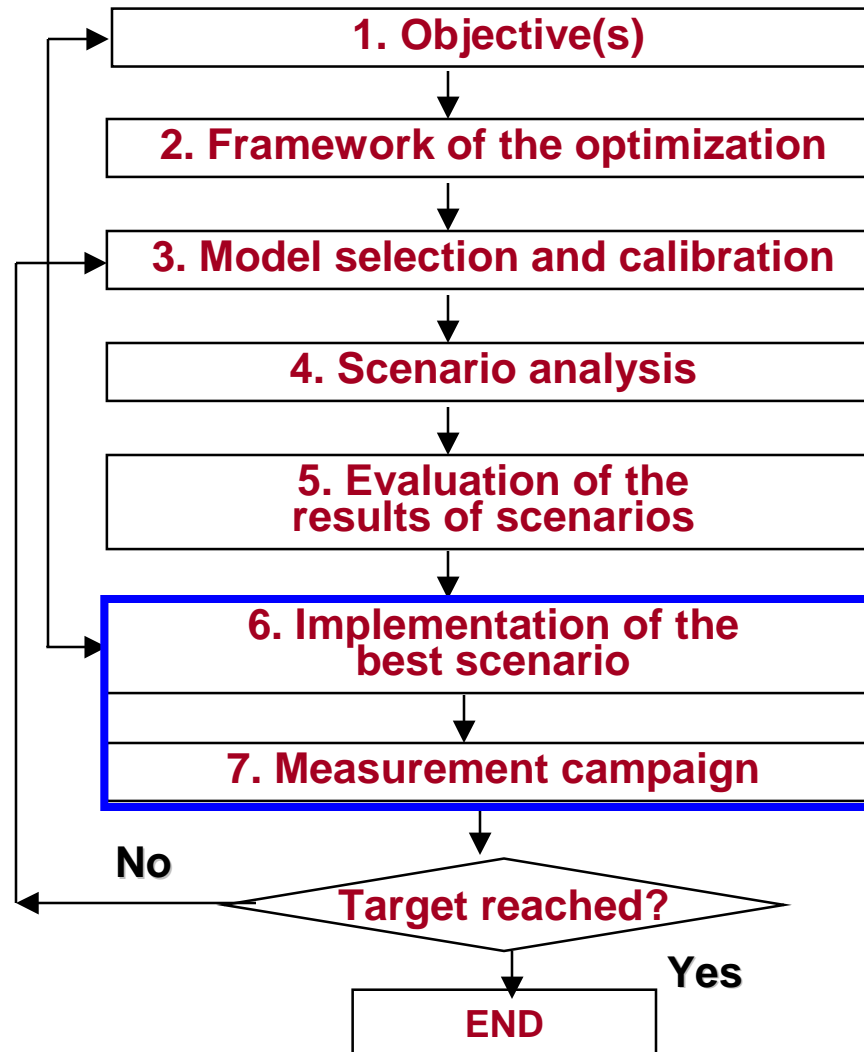


Total Nitrogen: 50% lower

PO₄ conc. < 1 mg/l



Systematic optimisation protocol



Limitations of model-based optimisation

- Settling properties of activated sludge are not predicted by the model
 - No unified mechanistic model available to predict filamentous bulking or pin-point settling issues in activated sludge.
 - But expert knowledge may be incorporated at the decision making step to account for this unknown parameter
- Changing system operation may alter the microbial population thereby resulting in a change of the kinetic & stoichiometric parameters of the model.
 - To account for this, iterate the systematic calibration protocol & re-calibrate the model if necessary until the objective of the optimisation is satisfied.

Conclusions & Perspectives

- A systematic protocol for model-based optimisation of SBRs is developed and successfully evaluated at a lab-scale SBR to achieve optimal N & P removal.
- Step-feeding of influent improves denitrification
=> reduces negative $\text{NO}_3\text{-N}$ effect on P-removal
- Frequent intermittent aeration during react phase is positive for overall N & P-removal
- Unmodelled phenomena should always be considered
- The systematic protocol is made flexible and objective oriented which can be used for different activated sludge systems
- Software support makes such scenario evaluation easy.

Arigato !