



LCA and nutrient removal

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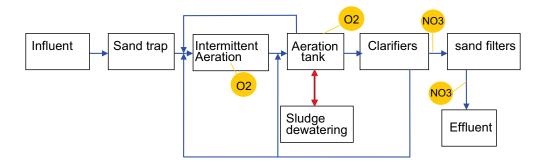
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- Online control for nutrient removal is standard practice at Aquafin (AQF) (Flanders)
- Goal of online control at Aquafin = meeting the effluent consent at the lowest cost
- Currently AQF has no stimulus to produce a cleaner effluent than strictly necessary since AQF doesn't pay a levy for the residual pollution
- A new methodology was assessed which sets as goal a reduction of the the footprint of wastewater treatment following a life cycle approach
- For this purpose, calibrated, asm2d models were made of 3 full scale WWTP's on which the two methodologies (costs respecting effluent consent versus lowest footprint) were compared



• Plant 1: 27.000 PE, limited online control already in place

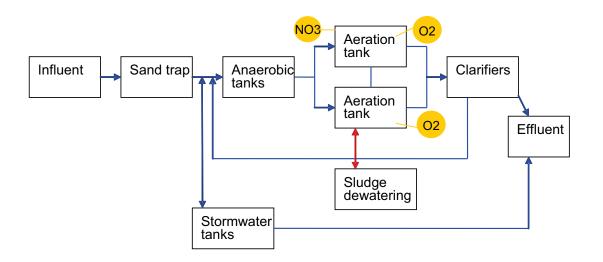


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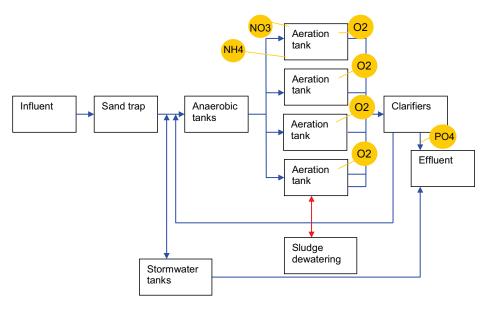


• Plant 2: 100.000 PE, online control of length of the aerated phase in place



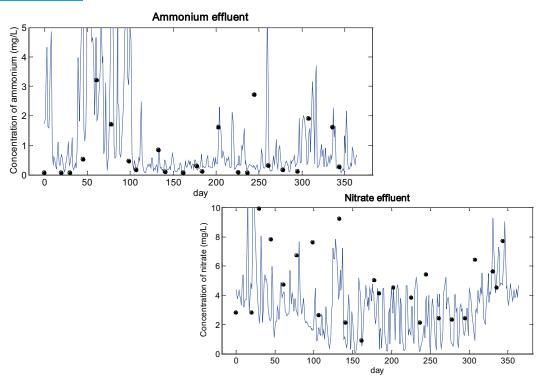


Plant 3: 270.000 PE, state of the art of online control at AQF



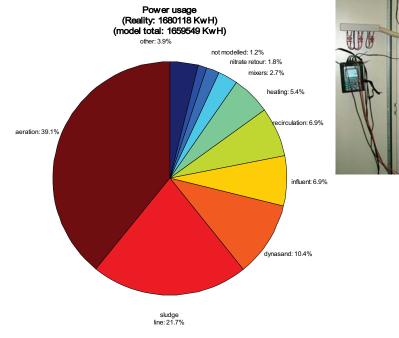
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Nepture Calibration



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Neptune Neptune

Comparison of optimisation strategies

Meeting effluent consent at lowest cost = straigthforward

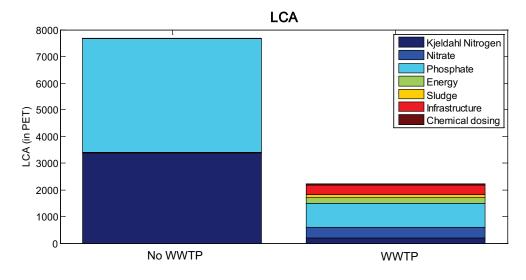
Reducing footprint of WWTP's

- Impact is expressed as mPET: milli people equivalents targeted. 1 PE represents the environmental impact of 1 hypothetical person in a defined country and year.
- Impact is composed of a number of impact categories such as global warming, eutrophication, acidification, ozone depletion, ecotoxicity, human toxicity, E.g. the EDIP97 methodology normalises the global warming impact of 1 PE to 8700 kg CO2-equivalents per year.
- Data from Henrik Fred Larsen:

| Parameter | Impact | |
|--|--|--|
| Nitrogen | 37,23 mPET / kg N | |
| Phosphorus | 269,2 mPET / kg P | |
| Electricity consumption | 0,12324 mPET / kWh | |
| Sludge production | 0,1 mPET / kg 37% DM sludge | |
| Infrastructure | structure 0,127 mPET / m³ influent treated | |
| FeCl ₃ 40% dosing | 2,611 mPET / kg | |
| Sodium acetate dosing 0,7781 mPET / kg NaOAc | | |

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Waste water treatment plants are lowering the ecological footprint (as expected..)



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- · Migration from manual to online control by installing extra online sensors
- Changing setpoints of existing controllers (NH4, SRT, O2, ...)
- Alternative (rule based) control algorithms
- Changing position of existing sensors
- Increasing internal recycle pumping capacity
- · For each plant roughly 2000 simulations were run



Results / Conclusions

| | | Cost optimisation | Footprint optimisation |
|---------|-----------|-------------------|------------------------|
| Plant 1 | Costs* | -15 % | -10 % |
| | Footprint | - 3 % | - 7 % |
| Plant 2 | Costs* | - 2 % | 0 % |
| | Footprint | - 13 % | - 22 % |
| Plant 3 | Costs* | - 7 % | - 2 % |
| | Footprint | - 7 % | - 11 % |

^{*} Sum of operational cost for electricity consumption, sludge disposal and chemical dosing

- Cost optimisation leads to a cost reduction of $2-15\,\%$ and an impact reduction of $3-13\,\%$
- Footprint optimisation leads to a cost reduction of 0 10 % and an impact reduction of 7 – 22 %
- Footprint optimisation leads to a cleaner effluent than the legally imposed quality, favours bio-P over chemical P removal and results into less NH4 in the effluent

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- A reduction of footprint with 1 % leads to an increase of operational costs with 1 %
- Standardisation of footprint calculation is necessary (!)
- Optimisation towards footprint is very compatible with the way operators tend to manually control the plants
- Online control reduces operational costs and increases treatment efficiency
- A plant that is already (partly) controlled online can perform even better if the correct controller settings are applied. These correct settings vary from plant to plant even when layouts are similar since every plant has its own characteristic influent composition.
- Custom made controllers are necessary to achieve the best performance

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Work package 4

LCA and ICA

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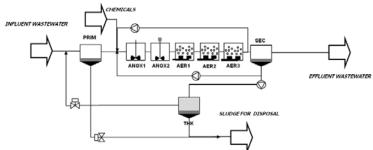






Neptune Simulation Benchmark

- A2O plant sized using the Metcalf & Eddy design guidelines
- The influent profile have been generated using phenomenological models including daily, weekly and seasonal variation (low C/N ratio)
- The EAWAG ASM3 bio P and the double exponential velocity function of Takács are the main process models

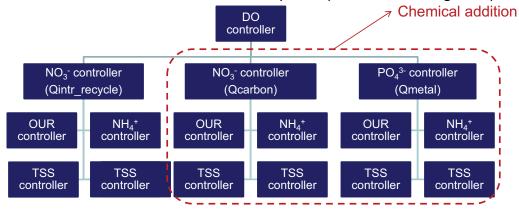


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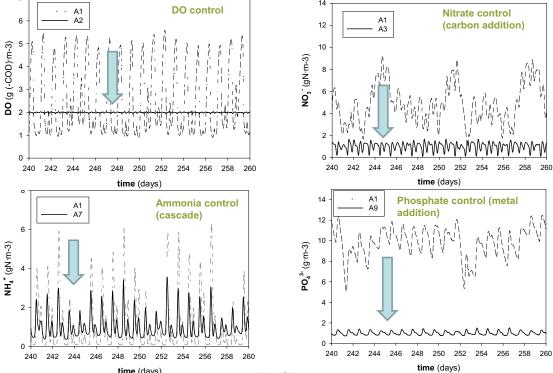
Evaluation of control strategies

- Different combinations of controllers tested using the Neptune Benchmark
- Comparison of strategies with and without chemical addition
- Is the implementation of control reducing environmental impact?
- Are the controllers based on the addition of chemicals the right solution to reduce environmental impact? (evaluation using LCA)





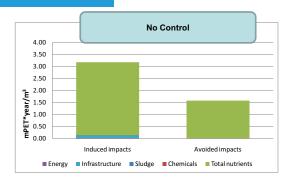
Results: dynamic profiles



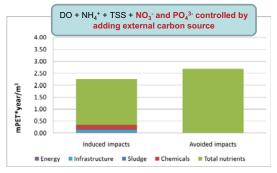
time (days)
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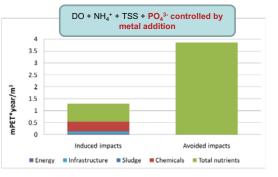
Neptune

Results: LCA evaluation









Avoided impact: Influent – effluent nutrient impact
Induced impact: Effluent nutrient + Electricity + Sludge + Infr + chemicals



- The implementation of control leads to an increase of the avoided impact and a decrease in the induced impact
- The most environmentally friendly strategies are the ones that include metal and carbon addition as they induce a significant reduction of nitrate and phosphorus in the effluent
- LCA gives better results for strategies that improve nutrient removal vs those that reduce energy consumption

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