

# Mitigating wastewater utility GHG footprints – Development of a Benchmark Simulation Model

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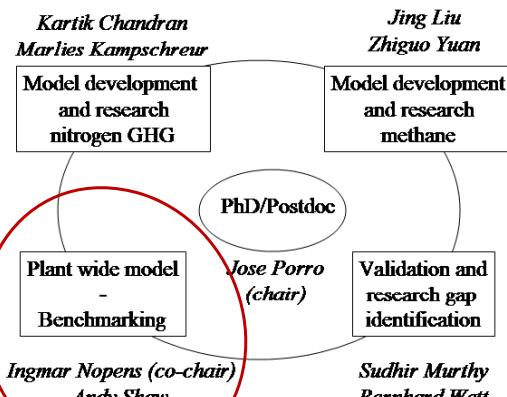


*Canada Research Chair  
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## IWA Task Group on GHG

- International voluntary collaboration under IWA umbrella
- Output = Scientific and Technical Rpt.

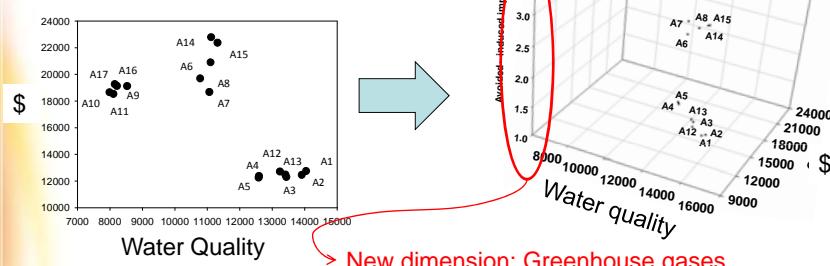


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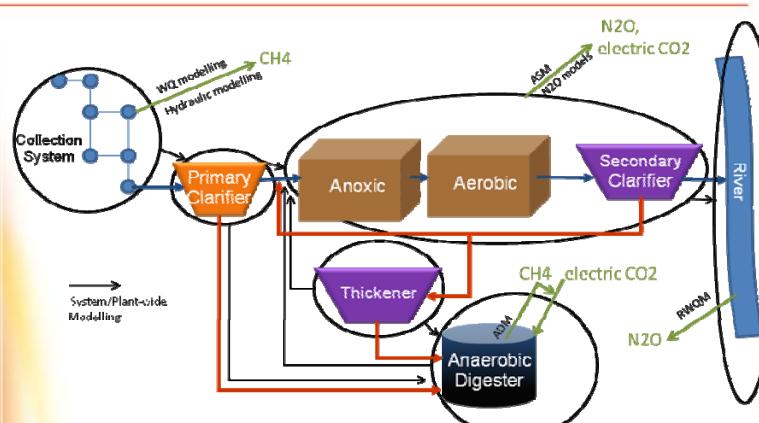


## Benchmarking concept

- Increasing demands on water quality at lower costs:
  - Development of new technologies and
  - Implementation of control strategies
- Evaluation of control strategies by using dynamic model simulation

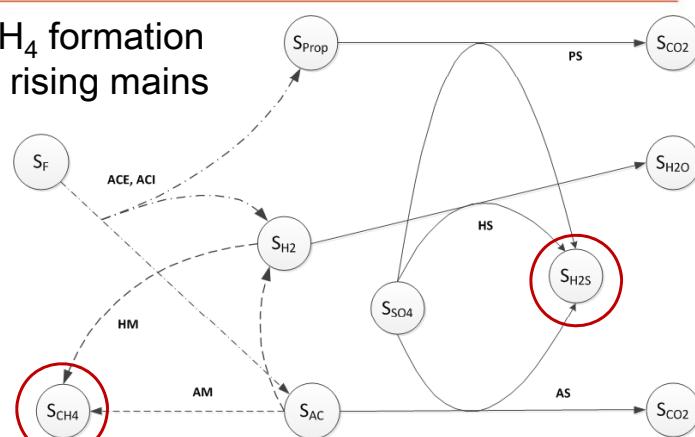


## Wastewater utility GHG



## GHG in sewer systems

- CH<sub>4</sub> formation in rising mains



Guisasola et al. (2009) Water Research 43: 2874-2884 5



## GHG in wastewater treatment

- N<sub>2</sub>O-formation during denitrification



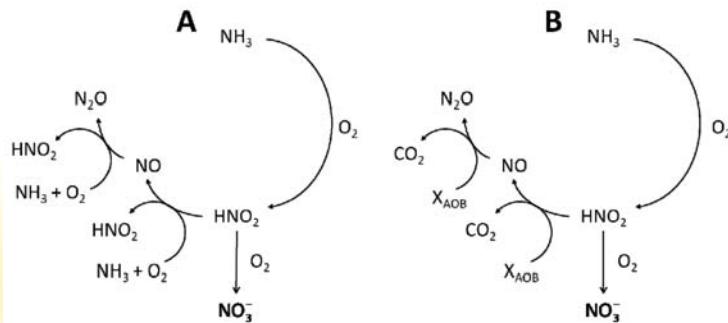
Hiatt & Grady (2008) Wat. Env. Res. 80: 2145-2156

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## GHG in wastewater treatment

- N<sub>2</sub>O-formation through nitrifier denitrification

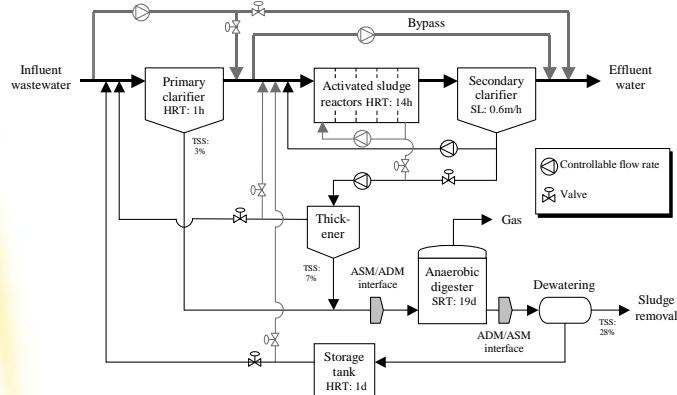


Mampaey et al. (2011) Nutrient recovery, Miami, Jan 2011



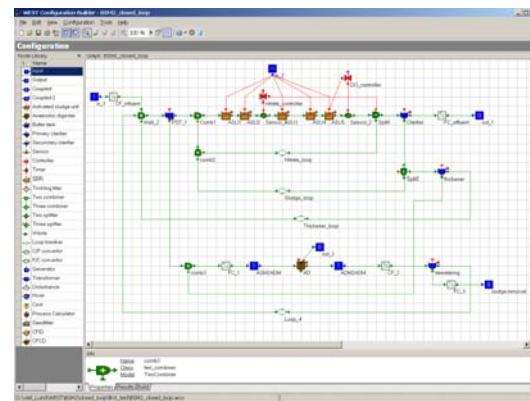
## Benchmark simulation platform

- BSM2 (IWA Task Group on benchmarking control strategies)



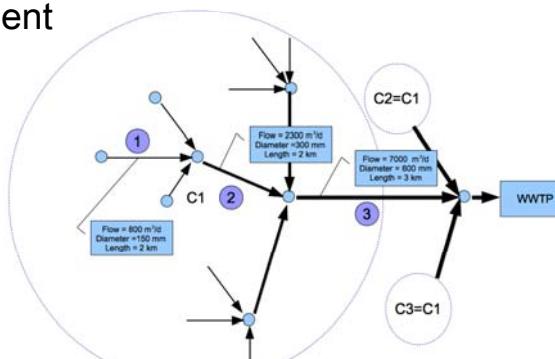
## Benchmark simulation platform

- BSM2GHG



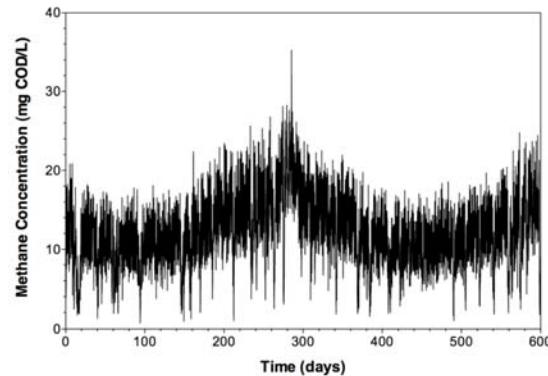
## Benchmark simulation platform

- Trunk sewer model (rising mains)
  - BSM2 influent
  - all CH<sub>4</sub> stripped at inlet pump station



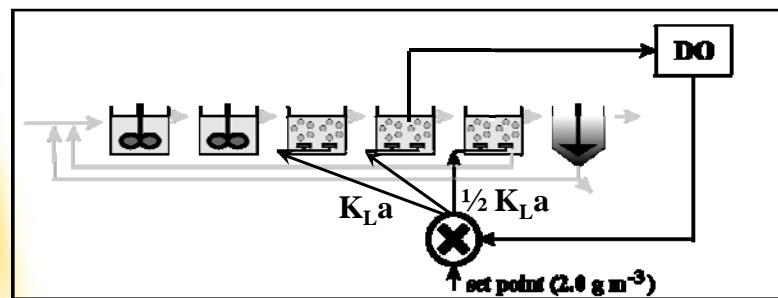
## GHG simulation results: Sewer

- CH<sub>4</sub> emissions at influent pump station



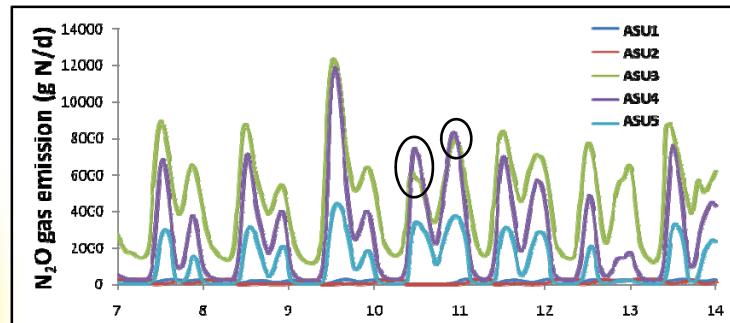
## GHG simulation results: WWTP

- Standard DO control in aerobic tanks



## GHG simulation results: WWTP

- Dynamics of N<sub>2</sub>O emissions in different tanks  
(none in anoxic, most in 1<sup>st</sup> (or 2<sup>nd</sup>) aerobic tank)



## GHG simulation results: WWTP

- Comparision of **no control** and **yes control** (DO control in aerobic reactor, DO = 2mg·L<sup>-1</sup>)

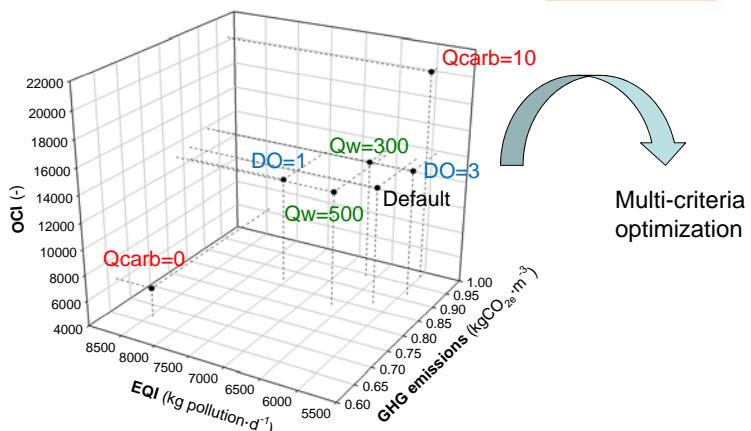
	No control	Yes control	%
Effluent Quality, EQI (kg poll·d <sup>-1</sup> )	6461	6181	-4
Costs, OCI (-)	14107	13254	-6
GHG emissions (kg CO <sub>2</sub> e·m <sup>-3</sup> )	0.975	0.860	-12

$$EQI = \frac{1}{t \cdot 1000} \int_{t_0}^{t_f} (a TSS + b BOD + c COD + d TKN + e NO3) Q dt$$

*OCI = Sludge production + Aeration + Pumping + Mixing  
+ Carbon addition + Heating – Methane production*



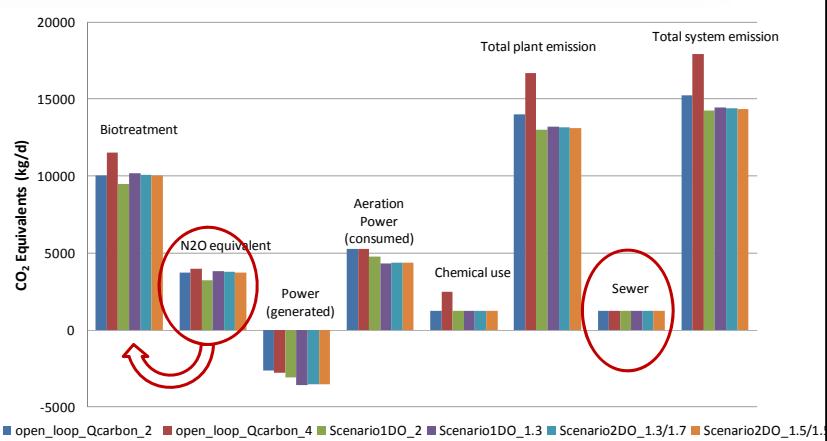
## GHG simulation results: WWTP



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## GHG simulation results: Integrated



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## Take home

- We are getting better at:
  - understanding GHG production and emission
  - understanding influencing process conditions
  - describing the processes in mathematical models
- We start using GHG process models to:
  - identify knowledge gaps
  - optimize process design and operation (control)
- We observe that:
  - A compromise must be sought between water quality, costs, greenhouse gas emissions

